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AN EXPERIMENTAL STUDY OF A CARBON-PHENOLIC ABLATION MATERIAL

by Kenneth Sutton

Langley Research Center

Hampton, Va. 23365

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# AN EXPERIMENTAL STUDY OF A CARBON-PHENOLIC ABLATION MATERIAL

## By Kenneth Sutton Langley Research Center

#### SUMMARY

An experimental ground-test program was conducted to evaluate the ablative characteristics of a carbon-phenolic heat-shield material designated Narmco 4028. The experimental results were compared with predictions from an ablation computer program. Tests were also conducted to evaluate the effects of hole patterns in the material and the effects of injecting water into the flow field through holes in the material. These latter tests were in support of a flight project called project RAM (radio attenuation measurements). The test facilities used in the investigation were the Langley 11-inch ceramicheated tunnel and the Langley 20-inch hypersonic arc-heated tunnel.

In the present tests, mechanical char removal of the material occurred for tests in air at model stagnation pressure above 2.4 atmospheres, but did not occur in nitrogen for pressures up to 11 atmospheres (1 atmosphere equals  $101.325 \ kN/m^2$ ). The mechanical char removal did not remove the entire char layer. An expansion of the material which can offset chemical removal also occurred, and there was an effect of fiber orientation. The experimental data showed that holes in the material can survive without enlargement and maintain their integrity. Water injected into the flow field through holes in the material had no significant effects on the behavior of the material and the holes remained free of any restrictions to the water flow during the tests.

The computer program used in the study was successful in predicting gross trends in material behavior. However, there was scatter in the comparisons between experimental and computer results which is attributed to phenomena, such as mechanical char removal, material expansion, and material degradation during cooldown, which could not be accounted for in the computer program.

#### INTRODUCTION

An experimental ground-test study was undertaken to evaluate the ablative characteristics of a carbon-phenolic heat-shield material. The material studied is designated Narmco 4028, a composite of 50 percent by weight of carbon fibers and 50-percent phenolic resin. The purpose of the present study was twofold.

First, the Langley Research Center has a continuing program of ground-test studies to investigate various types of ablators for possible use as heat shields for reentry flight application. Also, the experimental results are used to evaluate the ability of analytical computer programs to predict the ablative response of various materials. For this objective, models of Narmco 4028 material were tested in ground facilities over a range of aerodynamic conditions to obtain experimental results of char recession, thermal degradation of virgin material, char retention, back-surface temperature rise, surface temperature, fiber orientation effects, and observation of possible peculiarities of the material. The experimental results were compared with analytical computer predictions.

Second, the Narmco 4028 material is used as the heat shield at the nose region for some of the reentry flight vehicles in the project RAM (radio attenuation measurement) series at the Langley Research Center. Project RAM is investigating the blackout phenomena of radio communications encountered during atmospheric reentry and makes extensive use of flight vehicles to obtain experimental data. (See refs. 1, 2, and 3.) The requirements of the flight experiment imposed a unique feature for this heat shield. Water is injected through patterns of holes in the Narmco 4028 material into the flow field during the flight experiment. The results from the present study were part of the flight verification of the Narmco 4028 material for the RAM series. In addition to the necessity of knowing the general ablative behavior of Narmco 4028, tests were conducted to study the effects of holes in the material and the effects of water injection on the ablative behavior of the material. A full-scale replica of the RAM heat shield was tested in a rocket-engine exhaust as additional flight verification and the results of that test have previously been published in reference 4.

The test facilities used in the present study were the Langley 11-inch ceramicheated tunnel and the Langley 20-inch hypersonic arc-heated tunnel. The range of stagnation enthalpy was 1100 to 11 000 Btu/lbm (2.55 to 25.50 MJ/kg) and the range of model stagnation pressure was from 0.07 to 11 atmospheres. Stagnation heating rates were obtained from 130 to 1600 Btu/ft2-sec (1.48 to 18.20 MW/m $^2$ ). These ranges are for each parameter and are not inclusive of the other parameters.

#### SYMBOLS

The units used for the physical quantities defined in this paper are given both in the U.S. Customary Units and in the International System of Units (SI). (See ref. 5.)

H<sub>S</sub> stagnation enthalpy, Btu/lbm (MJ/kg)

K<sub>O</sub> mass fraction of oxygen in test stream

length of test model, in. (cm) l total cold-wall oxygen mass flux,  $\frac{q_s K_0 t}{H_c}$ , lbm/ft<sup>2</sup> (kg/m<sup>2</sup>)  $M_{O}$ stagnation-point pressure, atm  $p_{S}$ stagnation-point cold-wall heating rate, Btu/ft<sup>2</sup>-sec (MW/m<sup>2</sup>)  $\dot{\mathbf{q}}_{\mathbf{S}}$ approximate equilibrium stagnation-point surface temperature, OR (K)  $T_{S}$ t time, sec (s) ŵ flow rate of injected water, lbm/sec (kg/s) char thickness, in. (cm)  $x_c$ 

Primed symbols refer to computer results.

#### TEST FACILITIES

The test facilities used in the present investigation were the Langley 11-inch ceramic-heated tunnel and the Langley 20-inch hypersonic arc-heated tunnel. In figure 1, the approximate test conditions for a 1-inch-diameter (2.54-cm) hemispherical model are shown. Tests using air, nitrogen, and air-nitrogen mixtures as the test environment were conducted. The test conditions for the individual tests are given in tables I to IV.

The Langley 11-inch ceramic-heated tunnel was used for the test at higher pressures (6 to 11 atmospheres) although the facility has a low enthalpy capability. In this facility the test gas is heated by flowing through a pebble-bed heat exchanger before expanding through the nozzle. A free-jet Mach 2 nozzle with a 1.33-inch-diameter (3.38-cm) exit was used for the tests. The description and operating conditions of this facility with the Mach 2 nozzle is given in reference 6.

A wider range of test conditions and higher enthalpies could be obtained in the Langley 20-inch hypersonic arc-heated tunnel. The maximum model stagnation pressure in this facility is 3 atmospheres. This facility uses a rotating, radial, dc electric arc to heat the test gas. Three separate nozzles with exit diameters of 2.0, 3.3, and 6.6 inches (5.08, 8.38, and 16.76 cm) were used for this study. A description of this facility is given in reference 7.

#### MATERIAL AND MODEL DESCRIPTION

Narmco 4028 is a composite material of 50 percent by weight of phenolic resin and 50 percent of 1/4-inch (0.63-cm) carbon fibers. The nominal density of the virgin material is  $87 \text{ lbm/ft}^3$  (1392 kg/m³). An elemental chemical analysis for the nondegraded material is given in table V. As part of the present study, steady-state measurements of the thermal properties of the nondegraded and charred material were performed under contract. These results are given in reference 8.

The molding and curing of the commercially supplied molding compound were performed by the Langley Research Center. The size of the molded billets was approximately 12 inches (30.48 cm) in diameter and 4 inches (10.16 cm) thick. The carbon fibers will have a preferred orientation depending on method of molding. This preferred orientation has been noted in reference 9 for similar carbon and graphite composite materials. In the present billets the length of the fibers were alined perpendicular to the direction of the applied pressure during the molding operation. This fiber alinement is illustrated by the sketch in figure 2.

Several model designs were used in the present investigation. Most of the models were machined from the molded billets described. The models shown in figure 3 were used to study the general behavior of the material and its char. For each nose shape, models were made so that the carbon fibers were alined both perpendicular and parallel to the direction of the free-stream flow during the tests.

The effect of fiber orientation was further investigated by the use of the model design shown in figure 4. The test specimen of Narmco 4028 was bonded to a shell made of mild steel. (See fig. 4(a).) Models of this design were made, with orientation of the fibers in the test specimen being perpendicular, parallel, and shingled with respect to the flow of the test stream. (See fig. 4(b).) A special mold and molding technique was used to obtain the shingled orientation of fibers.

The hemispherical models with perpendicular-fiber orientation shown in figure 3(a) were used to investigate the effect of holes in the material. Holes were drilled in the models in three patterns as shown by the photographs in figure 5. The holes in the 1-hole pattern and the 4-hole pattern were 0.06 inch (0.15 cm) in diameter; whereas, the holes in the 13-hole pattern were 0.03 inch (0.08 cm) in diameter. The depth of the holes in all three patterns was approximately 0.6 inch (1.5 cm).

The model design shown in figure 6 was used for the tests of the effects of water injection. The test specimen had shingled-fiber orientation (fig. 4(b)) and was bonded to a mild steel holder with passages for the injection of water. Holes with diameters of 0.046 inch (0.117 cm) were located at the stagnation point and at  $60^{\circ}$  and  $81^{\circ}$  from the

stagnation point. As shown in figure 6(a), only the stagnation-point holes were connected to the water passage for the models used to study stagnation-point injection. For side injection, both the 60° and 81° holes were connected to the water passage. (See fig. 6(b).)

The model design shown in figure 7 was used in the measurement of back-surface temperature rise for the material. The test specimens (fig. 7(a)) were machined from the molded billets with both perpendicular- and parallel-fiber orientation. As shown in the assembly drawing (fig. 7(b)), a calorimetric plate of 1/64-inch-thick (0.04-cm) copper with three 30-gage chromel-alumel thermocouples is bonded to the back surface of the test specimen. The nose assembly is bonded to a cylindrical steel holder protected with a phenolic-cork composite. At the more severe test conditions, the cylindrical sidewalls were further protected by wrapping with fiber-glass tape. Reference 10 used this model design for similar tests.

#### TEST PROCEDURE AND INSTRUMENTATION

The test procedure was basically the same for all models in each of the two facilities. The test environment would be set by standard facility procedure; after the equilibrium stream condition was obtained, the model would be inserted into the test stream for the particular exposure time. At the end of exposure time the model would be retracted from the stream. For the tests in the ceramic-heated tunnel, a stream of argon was sprayed over the model to quench flaming of the model after retraction from the test stream.

The length of the test specimen was measured before and after the test. The specimens were sectioned after testing for further study; the studies included measurement of the depth of degradation of the material (that is char thickness).

The response of the model thermocouples was recorded on an oscillograph. Surface temperature of the model was measured with a photographic pyrometer. This type of instrument is described in reference 11; however, a more advanced photographic pyrometer than those described in reference 11 was used in the present tests and the temperature range of this type of instrument has been extended to 7000°R (3900 K). Motion-picture cameras with speeds up to 400 frames per second were used to record the behavior of the models during a test. The models could also be visually observed during a test.

The stagnation enthalpies and stagnation pressures for the tests in the ceramic-heated tunnel were taken from the results of reference 6. The heating rates were calculated by using these parameters and the heating-rate equations of reference 12. The oxygen mass fractions were measured with a calibrated choked orifice system used to mix the air and nitrogen. For the tests in the hypersonic arc-heated tunnel, the heating rates and stagnation pressures were measured with thin-wall calorimeters and pressure probes

respectively. These parameters were then used to calculate the stagnation enthalpies by the heating-rate equations of reference 12. The oxygen mass fractions were calculated from a known volumetric mixing of air and nitrogen.

For the water-injection tests, an instrumentation console was used which incorporated all the instruments necessary to control and record the water injection rates properly. The source of the water supply was a container filled with water and pressurized by air.

#### RESULTS AND DISCUSSION

The results of the individual tests are given in tables I to IV. In these tables are listed the stagnation-point length change, the char thickness, and the approximate equilibrium, stagnation point, surface temperature of the models for each test condition. For the model length change, a negative sign (-) refers to a recession of the model and a positive sign (+) refers to an expansion of the model. The char thicknesses are only given for those cases where the thermal degradation of the virgin material could be attributed to one-dimensional heat conduction.

#### Mechanical Char Removal

Mechanical char removal of the material was observed to occur at certain test conditions for air and air-nitrogen mixtures but not in nitrogen as noted in the result tables. This mechanical char removal is defined as pieces of char being removed from the char surface. For the tests in which mechanical char removal occurred, pieces of char would be observed leaving the surface of the model and the models did not retain a smooth char surface. The observation of mechanical char removal was made visually both during the tests and from the motion-picture films of the tests. The mechanical char removal of some representative tests is shown in figure 8 by photographs taken from the motion-picture films.

The regime of mechanical char removal is shown by the data in figure 9 and photographs in figure 10. These data are for the model designs shown in figure 3 with perpendicular-fiber orientation. Mechanical char removal did not occur in nitrogen over the entire test range nor in air and air-nitrogen mixtures at stagnation pressures below 2 atmospheres. At stagnation pressures greater than 6 atmospheres, mechanical char removal occurred whenever oxygen was present in the test stream. For air environments ( $K_0 = 0.23$ ), mechanical char removal occurred at stagnation pressures as low as 2.4 atmospheres.

The mechanical char removal for the material is a surface phenomenon and the entire char layer is not removed. Photographs of sectioned models are shown in

figure 11. As can be seen from the photographs, there is a thick char layer present even though severe mechanical char removal had occurred.

The cause of the mechanical char removal was not determined in the present tests. Char removal by aerodynamic shear is one possible mechanism. However, tests in nitrogen at stagnation pressures as high as 11 atmospheres and aerodynamic shears of 62 lbf/ft² (2.97 kN/m²) did not show any mechanical char removal. Mechanical char removal did occur at these test conditions in air and in air-nitrogen mixtures. Therefore, aerodynamic shear by itself is not considered the cause of the removal. In reference 13 is presented a theory for multidimensional gas flow through permeable char layers and this theory shows that an inflow of gas from the boundary layer into the char layer is possible. The inflow of a gas containing oxygen could oxidize and weaken the interior structure of the char to such an extent that mechanical char removal by aerodynamic shear is then possible. The present tests had the favorable conditions of small models, high pressures, and thick char layers for gas inflow as presented in reference 13. This concept of a weakening of the char due to gas inflow is only suggested as a possible mechanism and was not proven in present tests. However, the presence of oxygen has a definite influence on the initiation of the char removal.

#### Recession-Rate Data

Good recession-rate data for chemical removal of the char were not obtained in the present tests. At the higher pressure conditions the mechanical char removal was super-imposed on the chemical removal. Also, over the entire range of test conditions, there was a measurable expansion of the material which offset recession. In many of the tests, the length of the model was greater after the test than before the test. This expansion of the material occurred for all model designs. An attempt to correlate the expansion with various parameters was unsuccessful. Because of this mechanical removal and material expansion, a good experimental comparison could not be made with chemical-removal theories for the char even though the model surface temperatures were in the range usually associated with diffusion-controlled oxidation and sublimation of the char.

#### Fiber Orientation

The direction of the orientation of the carbon fibers with respect to the test stream flow has an effect on the ablative behavior of the material. In figure 12 are shown photographs of representative models after testing with fiber orientation perpendicular and parallel to the free-stream flow. Crevices are formed in the char layer at the nose region of the models with parallel-fiber orientation. This effect was not noted for any of the perpendicular-fiber models. Also, the recessions of the models with parallel-fiber orientation were always greater than those of the perpendicular-fiber models for

comparable test environments. In figure 13 is shown the comparison of stagnation-point length change between parallel and perpendicular fibers at comparable test conditions.

The model design shown in figure 4 was used to study further the effect of fiber orientation. In figure 14 representative models with the three different fiber orientations are shown. Again, crevices are formed at the nose region of the models with parallel-fiber orientation. No crevices were formed for the models with perpendicular- or shingled-fiber orientation. Also, the perpendicular- and shingled-fiber models have the same general response to an environment. There was no apparent mechanical char removal along the sidewalls of the models in any of the tests, regardless of the type of fiber orientation.

The crevices formed in the char layer for the parallel-fiber orientation do not extend into the nondegraded material. Even the most severe crevices did not extend past the pyrolysis interface. Also, the pyrolysis interfaces for these models have the same contour as the general contour of the exterior surface of the model.

#### Hole Patterns

The effect of holes in the material was studied at both high- and low-pressure conditions. No enlargements of the holes occurred in any of the tests as illustrated by the photographs in figure 15 for the highest pressure test condition and for severe mechanical char removal. The present experimental results indicate that holes can survive and maintain their integrity in the Narmco 4028 material.

At test conditions where models without holes did not have any mechanical char removal, the models with hole patterns also did not indicate any mechanical char removal. In the test regime for mechanical char removal, there is an effect of hole pattern on the stagnation recession of the models. In figure 16 the stagnation-point recession is shown for models with hole patterns tested at the highest pressure condition. At the longer test times there is greater recession for the models with hole patterns of 4 and 13 holes. The holes for the 4-hole model were located at the region of maximum shear.

#### Water Injection

The effect of water injection on the behavior of the Narmco 4028 material was investigated at both a high-pressure and a low-pressure test condition. In these tests the water was injected into the flow field either from an orifice at the stagnation point of the model (stagnation-point injection) or from two orifices at 60° and 81° from the stagnation point of the model (sidewall injection). The initiation of water injection was only after the model had reached a high surface temperature. The water was then

injected in pulses of 0.2 second on and 0.3 second off for the duration of the test. During the RAM flight experiments the water will also be injected in pulses. The flow rates of the injected water for each test are given in table III. Photographs of representative models during the test and after testing are shown in figures 17, 18, and 19. The stagnation-point surface temperatures were 4100° R (2278 K) for the models tested at the high-pressure condition and 5300° R (2944 K) for the low-pressure condition. Therefore, the models had a high surface temperature for any possible reaction with the water. For stagnation-point injection, the stagnation region of the model was cooled to a much lower temperature during the injection pulse, but the temperature was regained between the water pulses.

The basic behavior of the material for the water-injection tests was approximately the same as that for the tests without injection at comparable test conditions. The water injection neither increased nor decreased the effects of mechanical char removal. The stagnation-point length changes of the water-injection models were comparable with those obtained for the models without injection. Also, the holes in the material remained free of any restrictions to the water flow during the tests and the holes were clear after the tests.

#### Crack Formation

Another feature observed in the present tests was the formation of cracks in the virgin material for the model design shown in figure 3. The cracks developed only in the models with perpendicular-fiber orientation. Examples of these cracks are shown in figure 11. The cracks did not always extend to the exterior surface of the models. The models constructed with thinner material (figs. 4, 6, and 7) did not show any cracks.

#### Model Flaming

As previously noted in the section "Test Procedure and Instrumentation," a stream of argon was sprayed over the models to quench flaming of the model after retraction from the test stream for the tests in the ceramic-heated tunnel. Preliminary tests showed severe flaming due to combustion of pyrolysis gases (from continued degradation of the virgin material) with the atmospheric environment. A photograph taken from motion-picture film of a preliminary test is shown in figure 20 and illustrates the degree of flaming that would continue from 3 to 5 minutes after model retraction from the stream. The spraying with argon stopped this flaming during the actual test program.

#### Comparison with Computer Predictions

A study was made of the comparison between the experimental results and the predicted results from an ablation computer program. A description of the computer

program is given in reference 14. The computer predictions were only made for the stagnation region of the models. The results from the computer predictions for a particular test model are given in tables I, II, and IV. Computer predictions were not made for the models with parallel-fiber orientations because of the formation of the crevices. For the model design used to measure back-surface temperature rise (see fig. 7), the parallel-fiber specimens split during testing. Neither the change in nose shape of the model nor material expansion was taken into account in the computer predictions.

The thermal properties used for the computer predictions as presented in this report are given in table VI. A discussion of the sources of the properties is given in the appendix. Other combinations of thermal properties were studied; however, the present properties were better or as good as any of the various combinations.

In the computer predictions, the computations were continued until cooldown and the aerodynamic inputs were removed after the models were retracted from the stream. Effects of quenching the models with argon for the tests in the ceramic-heated tunnel were not taken into account in the computer predictions. The computer results showed that significant thermal degradation of the virgin material could occur after model retraction from the stream during the cooldown period. This continued degradation was up to 0.10 inch (0.25 cm) for the model design of figure 3 and the virgin material was always completely degraded for the model design of figure 7. The differences between the stagnation-point char thicknesses at the end of model exposure time and the end of the cooldown period are shown in figure 21.

Some typical comparisons between the experimental results and the computer predictions are shown in figures 22, 23, and 24 for the stagnation point. Although some of the results show good comparison, there is no consistency in the comparisons. In figure 25 the stagnation-point length changes of the models from the experimental and computer results are plotted as functions of total cold-wall, oxygen mass flux. As shown in figure 25(a), the length changes from the computer predictions can be adequately described with a linear least-square curve over the range of total oxygen flux. The experimental and calculated results show the same gross trend (that is  $\Delta l$  increasing with  $M_0$ ) but the computer results overpredicted model recession at low values of  $M_0$  (where many models showed a length increase due to swelling) and, in several instances, significantly underpredicted recession when mechanical char failure occurred. The comparisons of stagnation-point char thicknesses between the experimental data and the computer predictions are shown in figure 26. The experimental char thicknesses were always greater than the computer predictions for end of model exposure time (fig. 26(a)) but had a better comparison for end of the cooldown period (fig. 26(b)). In figure 27 is shown the

comparison between the experimental data and the computer predictions for the model stagnation-point surface temperature. There is a fair agreement, the experimental temperatures being slightly higher.

Some of the experimental results could be adequately described by the ablation computer program. However, over the range of experimental results, the computer program could not adequately describe the behavior of the material. This lack of agreement is attributed to the behavior of the material during mechanical char removal, material expansion, and continued degradation during cooldown which could not be accounted for in the present analysis. Because some tests were adequately predicted by the ablation program but not the entire test series, the present study has indicated that computer predictions illustrating material behavior and defining thermal properties which are based on comparisons with a few experimental tests should be viewed with caution.

#### CONCLUDING REMARKS

An experimental ground-test study was conducted to evaluate the ablative characteristics of a carbon-phenolic heat-shield material designated Narmco 4028. The experimental results were compared with predictions from an ablation computer program. In addition to the study of the general ablative behavior of the material, tests were also conducted, in support of project RAM, to evaluate the effects of hole patterns in the material and the effects of injecting water through holes in the material into the flow field.

In the present tests, mechanical char removal did occur at certain test conditions depending on the mass fraction of oxygen in the stream and the stagnation pressure. For tests in nitrogen at model stagnation pressures up to 11 atmospheres (limit of the tests), the mechanical char removal did not occur. The mechanical char removal did occur for tests in air at pressures above 2.4 atmospheres and air-nitrogen mixtures above 6 atmospheres. This mechanical char removal occurred at the surface of the char and did not remove the entire char layer.

The study showed that expansion of the material occurs during testing which tends to offset the recession due to chemical removal. There is an effect of fiber orientation on the material's behavior. The models with parallel-fiber orientation formed crevices during testing and had greater recession than the models with perpendicular-fiber orientation.

The experimental data showed that holes can survive without enlargement and maintain their integrity in the material. Water injection had no significant effects on the behavior of the material in these specific tests and the holes remained free of any restrictions to the water flow.

The computer program used in the present study was successful in predicting gross trends in material behavior and for several isolated tests it gave good predictions for detailed material response. Over the broad range of experimental conditions, however, comparisons between experimental and computer results showed considerable scatter. This scatter is attributed to phenomena, such as mechanical char removal, material expansion, and material degradation during cooldown, which was not accounted for in the computer program.

Langley Research Center,
National Aeronautics and Space Administration,
Hampton, Va., July 6, 1970.

#### APPENDIX

# SOURCES OF THE THERMAL PROPERTIES USED IN THE COMPUTER PREDICTIONS

The specific heats for the virgin material and the char were taken from reference 8. The thermal conductivities of the virgin material and the char depends upon the direction of the heat flow with respect to fiber orientation as shown by the data of reference 8. The selected thermal conductivities are based on the data of reference 8 for heat flow perpendicular to the fiber length (across fiber) which corresponds to the direction of heat flow at the model's stagnation region for perpendicular-fiber and shingled-fiber orientation of the present study. The thermal conductivity of the virgin material is taken directly from reference 8 and the thermal conductivity for the char is one-half the values given in reference 8.

The density of the virgin material was measured in the present study. There is a disagreement between measurements of the char density from reference 8 and the present study. Reference 8 gives measured char densities of 64 lbm/ft $^3$  (1025 kg/m $^3$ ) for char formed in a furnace and 74 lbm/ft $^3$  (1185 kg/m $^3$ ) for chars formed in a plasma jet. In the present study, a density of 74 lbm/ft $^3$  (1185 kg/m $^3$ ) was measured for chars formed in a furnace and densities from 57 to 68 lbm/ft $^3$  (913 to 1089 kg/m $^3$ ) for chars from several test models. Therefore, a density of 62 lbm/ft $^3$  (993 kg/m $^3$ ) was selected for the present study.

The heat of pyrolysis was determined from measured differential thermal analysis data. The rate constants for the thermal degradation of the virgin material was determined from measured thermal gravimetric analysis data.

The emissivity of the char was taken from the data of reference 8. The heat of combustion of the char was selected as a 10 to 20 percent increase over the value of the heat of formation of carbon monoxide being formed from graphite and oxygen. The value of the heat of sublimation of the char was selected as an average value for the sublimation of graphite. The char surface kinetics were taken from reference 15 for the "slow" kinetics of graphite.

The specific heats of the pyrolysis gas were determined from chemical equilibrium calculations based upon the elemental analysis of Narmco 4028 and the char density. This type of calculation does not account for carbon deposition. The specific heats used in the computer predictions are average values for the pressure range of the experimental program.

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TABLE I.- TEST CONDITIONS AND RESULTS FOR THE MODELS USED IN THE STUDY OF THE GENERAL BEHAVIOR OF THE MATERIAL

[Model design shown in fig. 3; primed values are computer values]

———т	_	_				_	10	10		20	20	-	-	0	0	22	22	0	0	0	0	t	S.	0	9	0
	οK	3090	3370		3455	3430	3455	3455	3302	3035	2395	2870	2450	2580	2560	2085	2255	1840	1870	1780	2100	1		2100	2100	1980
Ts	O.R.	5560	0909	3580	6220	6170	6220	6220	5950	5460	4310	5170	4330	4640	4610	3750	4060	3310	3370	3210	3780		3720	3780	3780	3560
	cm	0.850	.818	.508	,843	,596	.758	844	.749	.736	.434	.483	.569	.561	.361	.394	.323	.477	.579	.620	.378	1	.336	.378	.422	.574
× ©	in.	0.335	.322	200	.332	.235	.298	.332	.295	.290	171.	.190	.224	.221	.142	.155	.127	.188	.228	.244	.149	-	.132	.149	.166	.226
	cm	0.645 0	.576	409	.523	.386	.462	.524	.569	.554	.315	.338	.442	.434	.262	.297	.277	399	.475	.514	.280	-	.259	.277	.320	.470
(a) (a)	in.	0.254 0	.227	191	506	152	182	506	.224	218	124	.133	174	171.	103	.117	109	.157	.187	202	110	1	.102	109	.126	.185
	cm	-0.132 0.	332	167	467	127	292	467	129	068	508	662	114	167	782	259	444	043	056	000	190	-	124	188	-,251	099
,10	in.	-0.052 -0	131	990.	.184	.050	.115	.184	.051	.028	.200	.261	.045	990*-	308	102	175	.017	.022	000	075	1	049	074	099	039
£ 5		0-	1	-		-	-				-		_							-		<u> </u>		<u> </u>	_	_
Computer	bi carcar	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes	No	Yes	Yes	Yes	Yes
Mechanical	removal	No	No	No	No	No	No	No	No	No	No	Yes	No	No	Yes	Yes	Yes	Yes	Yes	Ño	Yes	Yes	Yes	Yes	Yes	Yes
	οK	3090	3370	1870	3700	3760	3760	3760	1	3035	-	2480	2540	2595	-	2460	2655	2090	2090	1950	2255	2270	i	3960 2200	2323	2145
E	O.R.	2560	0909	3360	0999	6760	0929	0949	-	5460	1	4460	4560	4660	-	4430	4780	3760	3760	3510	4060	4080	-	3960	4180	3860
	cm	0.71	.71	.61	1	1	1	-	1	!	99.	1 1		i	.51	.46	.51	.43	.61	.58	.35	.76	1	-	-	1
×	ii.	0.28	.28	.24	1	-	ł	1	1	1	.26	1	1 1	-	.20	.18	.20	.17	.24	.23	.14	.30	1	-	1	1
	cm	+0.086	157	015	290	+.046	089	284	+.041	079	079	-1.138	+.063	+.094	404	135	348	+.025	+.018	+.056	+.056	102	+.043	035	+.025	+.127
20	in.	+0.034	062	900	114	+.018	035	112	+.016	031	031	448	+.025	+.037	159	053	-,137	+.010	+.007	+.022	+.022	040	+.017	014	+.010	+.050
<b>,</b>	 ၁	30.0	30.0	30.0	30.0	10.0	20.0	30.0	20.0	20.0	30.0	29.3	20.0	20.0	30.0	20.3	20.0	20.5	29.7	29.9	15.0	15.0	10.0	15.0	20.0	30.0
Fiber	orientation	ere Perpendicular	Perpendicular 30.0	Perpendicular :	nere Perpendicular 30.0	ere Perpendicular	ere Perpendicular 20.0	ere Perpendicular	Perpendicular 20.0	Perpendicular 20.0	Perpendicular 30.0	Perpendicular 29.3	Perpendicular 20.0	Perpendicular 29.9	ere Perpendicular	Parallel	Perpendicular	Perpendicular	Perpendicular	here Perpendicular 30.0						
Nose	shape	Hemisphere F	Hemisphere P	Hemisphere F	Hemisphere F	Hemisphere F	Hemisphere F	Hemisphere F	Hemisphere I	Blunt	Hemisphere I	ere		Hemisphere I	Hemisphere 1	Blunt	Blunt		Blunt	Blunt	Hemisphere 1	Hemisphere	Hemisphere	Hemisphere	Hemisphere	Hemisphere
	MW/m <sup>2</sup>	7.72		1.48	18.16	18.16	18.16	18.16	12.37	7.72	3.72	7.95	4.52	6.47	5.62	3.43	3.45	3.45	3,45	3.45	5.11	5,11	5.11	5.11	5.11	5.18
g	Btu/lbm MJ/kg Btu/ft2-sec MW/m2	680	1250	130	1600	1600	1600	1600	1090	089	328	700	398	570	495	302	304	304	304	304	450	450	450	450	450	456
trange i	MJ/kg	25.52	25.05	3.59	25.52	25.52	25.52	25.52	12.76	11.60	3.48	5.43	4.41	4.41	3.48	2.55	2.55	2.55	2.55	2.55	2.55	2,55	2.55	2.55	2,55	2.55
Hs	tu/lbm	11 000	10 800	1 550	11 000	11 000	11 000	11 000	5 500	2 000	1 500	2 340	1 900	1 900	1 500	1 100	1 100	1 100	1 100	1 100	1 100	1 100	1 100	1 100	1 100	1 100
		23		.23	.23		.23		80.	80.	.23	.23	80.	80.	.23	.13	.23	.02	.02	_	.08	*00	80.	80.	80.	.02
Ps,		0.07 0.		.43	09	.60	.60		1.08					2.50	2.91	5.88	5.97	5.97	5.97	5.97	6.05	6.05	6.05	6.05	6.05	6.13
	•	10	_									- 17	2	es/	64	43	43	43	-23					_	_	

<sup>a</sup>Char thickness at end of model exposure time. <sup>b</sup>Char thickness at end of cooldown period.

TABLE I.- TEST CONDITIONS AND RESULTS FOR THE MODELS USED IN THE STUDY OF THE GENERAL BEHAVIOR OF THE MATERIAL ~ Concluded

Ts-	οK	1	2190	2270	1	2140	. !	2155	2180	1860	2430	1	2040	1980	1	1880	!	2195	2195	2220	2250	2190	1
	e.	1	3950	4090	!	3860	-	3880	3930	3350	4380	-	3670	3560	-	3380	-	3950	3950	4000	4050	3950	-
	E S	1	0.343	.320	1	.374	-	.729	.358	.564	-	1	.595	.645		.292		.503	.302	.315	.325	.340	-
, × 5	ıı	-	0.135	.126	-	.147	-	.287	.141	.222	.083	1	.234	.254	1	.115	-	.198	.119	.124	.128	.134	-
	cm	-	0.244	.229	-	274	1	.595	.264	.432	.190	1	.465	.566	;	.221	-	.396	.200	.218	.231	244	-
, χ <u>α</u>	in.		0.096	060.	1	108	-	.234	104	.170	.075	-	.183	.223	-	.087	!	.156	620.	980.	160.	960.	-
	cm		-0.284 0	460	-	224		000	.348	000	885	:	137	000.	-	287	<u>.</u> 	061	.211	.318	427	297	
.20	in.	1	-0.112	.181	1	.088	1	000	.137	000	.348	-	054	000.	-	113	-	.024	083	.125	.168	117	<u> </u>
Computer	prediction	No -	Yes -0	Yes	No	Yes	No	Yes	Yes	Yes	Yes -	No	Yes -	Yes	No	Yes	No	Yes	Yes	Yes	Yes -	Yes	No
ī	ਢ	Yes	Yes	Yes	No	Yes	Yes	No	Yes	No	Yes	Yes	Yes	No	No	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes
Ts	OR OK	4110 2285	4300 2390		3330 1850	4180 2320	4180 2320	3720 2070	4160 2310	3580 1990	4730 2630	4550 2530	3780 2100	3780 2100	3810 2115	3840 2135	3760 2090	3960 2200	3810 2115	4360 2420	4160 2310	4290 2380	4310 2395
ပ	СШ	1	0.56	.61	.48	.46	.63	1	.46	.53	.41	30	-	-		.33	30	.53	1	Ì		.46	.46
×	in,	ŀ	0.22	.24	.19	.18	.25	:	.18	.21	.16	.12	1	-	-	.13	.12	.21	-	1	;	.18	.18
	cm	-0.173	023	-,434	104	091	246	+.046	612	+.046	-1.316	920	046	+.170	+.023	483	559	+.030	211	328	606	290	571
10	in.	-0.068	600	171	+.041	036	097	+.018	241	+.018	518	361	018	+.067	+.009	190	220	+.012	083	129	239	114	225
۾ پڻ آ	ر ا ا	30.0	15.2	20.1	25.2	15.2	12.1	39.4	20.1	20.2	20.2	20.0	30.7	30.7	30.4	15.7	15.2		10.0	15.0	20.0		15.0
Fiber	or remeation	Parallel	sphere Perpendicular	Perpendicular	Perpendicular	Hemisphere Perpendicular	Parallel	Perpendicular	Perpendicular	Perpendicular	Perpendicular	Parallel	sphere Perpendicular	sphere Perpendicular	Parallel	sphere Perpendicular	Parallel	Perpendicular 20.4	sphere Perpendicular 10.0	sphere Perpendicular	sphere Perpendicular 20.0	sphere Perpendicular 15.0	Parallel
Nose	Suape	Hemisphere	Hemisphere	Blunt	lunt	Hemisphere	Hemisphere		Blunt	unt	Hemisphere	Blunt	Hemisphere	Hemisphere	Hemisphere	Hemisphere	Hemisphere	Blunt	Hemisphere	Hemisphere	Hemisphere	Hemisphere	Hemisphere
	$\mathrm{MW/m^2}$	5.18	5.28	3.56	3.95	6.13	6.13	4.45	4.54	4.59	6.72	4.51	6.88	6.88	6.88	4.84	4.84	4.66	6.92	6.92	6.92	7.04	7.04
qs	$MJ/kg$ Btu/ft2-sec $MW/m^2$	456	465	314	348	540	540	392	400	404	592	397	909	909	909	426	426	411	610	610	610	620	620
	MJ/kg	2.55	2.55	2.55	2.55	2.55	2.55	2.55	2.55	2.55	2.55	2.55	2.55	2.55	2.55	1.91	1.91	2.55	2.55	2.55	2.55	2.55	2.55
Hs	Btu/lbm	1100	1100	1100	1100	1100	1100	1100	1100	1100	1100	1100	1100	1100	1100	822	822	1100	1100	1100	1100	1100	1100
							_		က	_	က	e2	2			6	60:	.02	10	10	10	60.	60
3		0.02	.12	.23	0	80.	90.	0	.13	0	.23	.13	.02	_	0	60.	۰,	۰.	Η.	Ξ.	Τ.	٩	٧.

 $^{\mathrm{a}}\mathrm{Char}$  thickness at end of model exposure time.  $^{\mathrm{b}}\mathrm{Char}$  thickness at end of cooldown period.

TABLE II.- TEST CONDITIONS AND RESULTS FOR THE MODELS USED TO STUDY THE EFFECTS OF FIBER ORIENTATION

Model design shown in fig. 4

										_ `			
T.s	Уо	-	3330	3260	1	2630	2620	-	2080	2080	1	2220	2220
H	OR	1		5860	1	.487 4740 2630	4710	-	3750	3750	-	290 4000 2220	4000
	cm	-	386	.348	-	.487	.460	-	.368	.343	1 2 3	.290	.310
, x <sub>c</sub> (a)	ij.	1	.152	.137	!	192	181	-	.145	.135	-	.114	.122
	cm	-	.359 0	.226	1 1 1	.322	308	-	.264	.249	-	.201	.208
(a)	in.		.102 0	680.	!	.127	.121	1	.104	860.	1	620.	.082
	cm		-0.018 -0.046 0.102 0.359 0.152 0.386 6000	033	-	204	180	-	203	188	-	295	318
.10		-	118 -0	013	;	082	071	_	- 080	074		116	125
	ii.	1	-0.0	-	;	;	·	-		-	-	7	7
Computer	prediction	No	Yes	Yes	No	Yes	Yes	No	Yes	Yes	No	Yes	Yes
Mechanical	removal	No	No	No	No	No	No.	Yes	Yes	Yes	Yes	Yes	Yes
s E	Уо		3310	3260	2700	2700	2590	- [	2220	-	2420	2545	2370
I	OR	İ	.51 5960	2860	4860 2700	4860	4660	-	4000	!	4360 2420	4580 2545	4260 2370
	cm	99.0		.41	1	1	!	1	.63	.56		-	-
×c	in.	0.26	.20	.16	-	-	1	1	.25	.22	-	-	1
	cm	-0.102	+.081	015	132	980'	107		091	107	1 1		470
10	in.	-0.040 -0.102 0.26 0.66	+.032	900'-	-,052	039	045	1	036	042	-		185
t, sec		9.3	4.5	3.6	12.5	16.2	14.3	14.3	16.5	15.4	12.5	14.2	15.2
Fiber orientation		Parallel	Perpendicular	Shingled	Parallel	Perpendicular 16.2	Shingled	Parallel	Perpendicular	Shingled	Parallel	Perpendicular	Shingled
	$MW/m^2$	18.16	18.16	18.16	6.81	6.81	6.81	5.11	5.11	5.11	6.93	6.93	6.93
đs.	Btu/lbm MJ/kg Btu/ft <sup>2</sup> -sec MW	1600	1600	1600	009	009	900	450	450	450	610	610	610
20	MJ/kg	25.52	25.52	25.52	4.53	4.53	4.53	2.55	2.55	2.55	2.55	2.55	2.55
Hs	3tu/lbm	11 000	11 000	11 000	1 950	1 950	1 950	1 100	1 100	1 100	1 100	1 100	1 100
М			.23	.23	.12	.12	.12	80.	80°	90.	.10	.10	.10
Ps,	arii	0.60 0.23	.60	9.	2.50	2.50	2.50	6.05	6.05	6.05	11.00	11.00	11.00

aChar thickness at end of model exposure time. bChar thickness at end of cooldown period.

# TABLE III.- TEST CONDITIONS AND RESULTS FOR THE MODELS USED TO STUDY THE EFFECTS OF WATER INJECTION

# [Model design shown in fig. 6]

	6.93	2.55     610     6.93       2.55     610     6.93       2.55     610     6.93	1 100         2.55         610         6.93           1 100         2.55         610         6.93           1 100         2.55         610         6.93	
01 02	6.93 6.93 6.93	2.55 610 6.93 2.55 610 6.93 2.55 610 6.93 9.55 610 6.93	1100     2.55     610     6.93       1100     2.55     610     6.93       1100     2.55     610     6.93       1100     2.55     610     6.93	.10 1100 2.55 610 6.93 .10 1100 2.55 610 6.93 .10 1100 2.55 610 6.93
	6.93	2.55 610 6.93 2.55 610 6.93 3.55 610 6.93	1100 2.55 610 6.93 1100 2.55 610 6.93 1100 2.55 610 6.93	.10 1100 2.55 610 6.93 .10 1100 2.55 610 6.93 .10 1100 2.55 610 6.93
	610 610 610	2.55 2.55 2.55	1 100 2.55 1 100 2.55 1 100 2.55	.10 1100 2.55 .10 1100 2.55 .10 1100 2.55

# TABLE IV.- TEST CONDITIONS AND RESULTS FOR THE MODELS USED IN THE MEASUREMENT OF BACKSURFACE TEMPERATURE RISE

# [Model design shown in fig. 7]

Ts	Уо	2080	2600	!	2540	3150	1 1
I	oR	3740	4680	-	4570	2670	-
	cm	1.270	1.270	1	.500 1.270 4570 2540	.500 1.270 5670 3150	-
, x, c, (b)	in.	0.500	.500	-	.500		-
. (	cm	0.653	797.	1	.772	.687	1
xc' (a)	in.	0.257	.314		.304	.269	1
_	cm	-0.037 -0.094 0.257 0.653 0.500 1.270 3740 2080	089 .314 .797 .500 1.270 4680 2600		081	125	
۱,7۵	in.	-0.037	035	!	032	049	
Computer		Yes	Yes	No	Yes	Yes	No
Note				Split			Split
_ თ	OK	2200	2680	2700	3005	3363	3105
Ħ.	cm in. cm <sup>0</sup> R	3960	4820	.50 1.27 4860 2700 Split	.50 1.27 5410 3005	.46 1.17 6060 3363	028 .49 1.24 5590 3105 Split
x <sub>c</sub>	cm	1.04	1.24	1.27	1.27	1.17	1.24
×	in.	0.41	.49				.49
	cm	+0.018	038 .49 1.24 4820 2680	+.005	008	094	
10	in.	+0.007	015	+.002	003	037	011
t, sec		62.2	61.0	45.0	57.5	35.5	28.2
Fiber orientation		Perpendicular 62.2 +0.007 +0.018 0.41 1.04 3960 2200	Perpendicular 61.0015	Parallel 42.0 +.002	Perpendicular 57.5	Perpendicular 35.5	Parallel 28.2
	$MW/\mathrm{m}^2$	1.45	3.24	3.52	3.06	7.05	7.44
qs	$Btu/lbm \hspace{0.1cm} MJ/kg \hspace{0.1cm} Btu/ft^2\text{-sec} \hspace{0.1cm} MW/m^2$	128	285	310	270	621	655
so.	MJ/kg	11.60	26.68	29.00	24.82	26.68	28.07
Hs	Btu/lbm	0.07 0.23 5 000 11.60	.07 .23 11 500	12 500	.23 10 700	.23 11 500	.23 12 100
Ϋ́		0.23	.23	.23		.23	.23
Ps, atm		0.07	.07	.07	.07	.32	.32

<sup>a</sup>Char thickness at end of model exposure time. bChar thickness at end of cooldown period.

#### TABLE V.- ELEMENTAL ANALYSIS OF NARMCO 4028

### [Percentages by weight]

Carbon		•		•		•	•	•				•	•	•	•	•	•	•	•	•		•	83.63
Oxygen																	•			•			10.79
Hydrogen	•	•				•			•	•							•	•					3.44
Nitrogen .	•					•	•												•				0.38
Ash				•		•	•				•						•			•		•	0.56
Total																							98.80

## TABLE VI. - THERMAL PROPERTIES USED IN COMPUTER PREDICTIONS (a) Virgin material

87 lbm/fi	$3 (1392 \text{ kg/m}^3)$
Density	R kJ/kg-K
	0.99
4000 TO (000 TC)	1.22
TOOL TO (AND TEXT)	1.33
000 m (00m yr)	1.39
TCCO TO (499 V)	1.45
0000 T (APP 77)	1.51
2000 - (500 77)	1.56
(500.77)	1.62
(044 77)	1.68
(TOO T)	1.80
14600 R (811 K)	- TT / TZ
Btu/ft-sec-	
(0.50 × 10	
(net xx)	
	4 0.693
0000 TO (APP IZ)	
000 T (FOO T)	4 0.774
(700.77)	
14000 TO (044 TV)	4 0.698
1000 7 (700 77)	
1260° R (700 K)	-4 0.479
1460° R (811 K)	m (0.465 MJ/kg)
Heat of pyrolysis	
Rate constants for thermal degradation:	$0 \times 10^{16} \text{ kg/m}^3 - \text{s}$
	(0.204 MJ/mole)
First frequency factor	$8 \times 10^{14} \text{ kg/m}^3 - \text{s}$
G and framework factor	
Second activation energy $5.01 \times 10^4$ calories/mole	

### TABLE VI.- THERMAL PROPERTIES USED IN COMPUTER PREDICTIONS - Continued (b) Charred material

Specific heat:         Btu/bm-OR         k1/kg-K           500° R (278 K)         0.240         1.00           1000° R (556 K)         0.330         1.38           1460° R (811 K)         0.335         1.61           1960° R (1099 K)         0.445         1.86           2460° R (1866 K)         0.480         2.01           2960° R (1645 K)         0.495         2.06           3460° R (1923 K)         0.505         2.11           3660° R (2200 K)         0.515         2.15           4460° R (2478 K)         0.520         2.17           4560° R (2756 K)         0.525         2.19           5460° R (3803 K)         0.525         2.19           5460° R (3803 K)         0.530         2.21           560° R (3807 K)         0.530         2.21           560° R (3807 K)         0.530         2.21           560° R (3807 K)         0.540         2.26           660° R (3807 K)         0.540         2.26           660° R (3807 K)         0.540         2.28           660° R (3807 K)         0.540         2.28           660° R (3807 K)         0.540         2.28           500° R (278 K)         0.540         2.28																		
Source   Care Ki	Density.			 	 	 										6	2 lbm/ft <sup>3</sup>	$(1184 \text{ kg/m}^3)$
1000°R (556 K)	Specific he	eat:														Btu	/lbm-0R	kJ/kg-K
1460° R (811 K)	500° R	(278 K)		 	 	 											0.240	1.00
1960° R (1098 K)	1000° R	(556 K)		 	 	 											0.330	1.38
2460° R (1865 K)																	0.385	1.61
2960° R (1945 K)	1960° R	(1089 K)		 	 	 											0.445	1.86
\$460° R (1923 K)																	0.480	2.01
3960° R (2200 K)	$2960^{\rm O}$ R	(1645 K)		 	 	 											0.495	2.06
4460° R (2478 K).       0.520       2.17         4960° R (2756 K).       0.525       2.19         5460° R (3331 K).       0.535       2.24         6460° R (3590 K).       0.540       2.26         6960° R (3867 K).       0.545       2.28         Thermal conductivity:       Btu/tr-sec-0R W/m-K         500° R (278 K)       0.13 × 10 <sup>-3</sup> 0.810         1000° R (556 K)       0.14 × 10 <sup>-3</sup> 0.872         1460° R (811 K)       0.15 × 10 <sup>-3</sup> 0.955         1960° R (1089 K)       0.16 × 10 <sup>-3</sup> 0.977         2460° R (1866 K)       0.18 × 10 <sup>-3</sup> 1.128         2960° R (1645 K)       0.18 × 10 <sup>-3</sup> 1.128         3210° R (1782 K)       0.21 × 10 <sup>-3</sup> 1.314         3460° R (1923 K)       0.21 × 10 <sup>-3</sup> 1.502         3960° R (1923 K)       0.21 × 10 <sup>-3</sup> 1.502         3960° R (2786 K)       0.24 × 10 <sup>-3</sup> 3.002         4460° R (2478 K)       0.43 × 10 <sup>-3</sup> 3.002         4960° R (3031 K)       0.48 × 10 <sup>-3</sup> 3.002         4960° R (3030 K)       0.78 × 10 <sup>-3</sup> 4.880         5660° R (3311 K)       0.70 × 10 <sup>-3</sup> 6.390         6400° R (3756 K)       0.70	$3460^{\rm O}~{ m R}$	(1923 K)		 	 	 											0.505	2.11
4960° R (2756 K)       0.525       2.19         5460° R (3030 K)       0.530       2.21         5960° R (3311 K)       0.535       2.24         6460° R (3590 K)       0.540       2.26         6660° R (3867 K)       0.545       2.28         Thermal conductivity:       Btu/ft-sec-OR       W/m-K         500° R (278 K)       0.13 × 10 <sup>-3</sup> 0.810         1000° R (556 K)       0.14 × 10 <sup>-3</sup> 0.972         1460° R (811 K)       0.15 × 10 <sup>-3</sup> 0.955         1960° R (1089 K)       0.16 × 10 <sup>-3</sup> 0.977         2460° R (1366 K)       0.18 × 10 <sup>-3</sup> 1.128         2960° R (1645 K)       0.18 × 10 <sup>-3</sup> 1.128         2960° R (1645 K)       0.19 × 10 <sup>-3</sup> 1.189         3210° R (1782 K)       0.21 × 10 <sup>-3</sup> 1.314         3460° R (1923 K)       0.21 × 10 <sup>-3</sup> 1.502         3960° R (2200 K)       0.33 × 10 <sup>-3</sup> 2.065         4460° R (2478 K)       0.43 × 10 <sup>-3</sup> 2.790         4710° R (2617 K)       0.48 × 10 <sup>-3</sup> 3.502         5460° R (3331 K)       0.56 × 10 <sup>-3</sup> 3.502         5460° R (3331 K)       0.56 × 10 <sup>-3</sup> 3.502         5460° R (3311 K)       0.70 <td>3960° R</td> <td>(2200 K)</td> <td></td> <td> </td> <td> </td> <td> </td> <td></td> <td>0.515</td> <td>2.15</td>	3960° R	(2200 K)		 	 	 											0.515	2.15
4960° R (2756 K)       0.525       2.19         5460° R (3030 K)       0.530       2.21         5960° R (3311 K)       0.535       2.24         6460° R (3590 K)       0.540       2.26         6660° R (3867 K)       0.545       2.28         Thermal conductivity:       Btu/ft-sec-OR       W/m-K         500° R (278 K)       0.13 × 10 <sup>-3</sup> 0.810         1000° R (556 K)       0.14 × 10 <sup>-3</sup> 0.972         1460° R (811 K)       0.15 × 10 <sup>-3</sup> 0.955         1960° R (1089 K)       0.16 × 10 <sup>-3</sup> 0.977         2460° R (1366 K)       0.18 × 10 <sup>-3</sup> 1.128         2960° R (1645 K)       0.18 × 10 <sup>-3</sup> 1.128         2960° R (1645 K)       0.19 × 10 <sup>-3</sup> 1.189         3210° R (1782 K)       0.21 × 10 <sup>-3</sup> 1.314         3460° R (1923 K)       0.21 × 10 <sup>-3</sup> 1.502         3960° R (2200 K)       0.33 × 10 <sup>-3</sup> 2.065         4460° R (2478 K)       0.43 × 10 <sup>-3</sup> 2.790         4710° R (2617 K)       0.48 × 10 <sup>-3</sup> 3.502         5460° R (3331 K)       0.56 × 10 <sup>-3</sup> 3.502         5460° R (3331 K)       0.56 × 10 <sup>-3</sup> 3.502         5460° R (3311 K)       0.70 <td>4460° R</td> <td>(2478 K)</td> <td></td> <td> </td> <td> </td> <td> </td> <td></td> <td>0.520</td> <td>2.17</td>	4460° R	(2478 K)		 	 	 											0.520	2.17
5960° R (3311 K)       0.535       2.24         6460° R (3590 K)       0.540       2.26         6960° R (3867 K)       0.545       2.28         Thermal conductivity:       Btu/ft-sec-°R       W/m-K         500° R (278 K)       0.13 × 10⁻³       0.810         1000° R (556 K)       0.14 × 10⁻³       0.872         1460° R (811 K)       0.15 × 10⁻³       0.935         1960° R (1089 K)       0.16 × 10⁻³       0.977         2460° R (1366 K)       0.18 × 10⁻³       1.128         2960° R (1645 K)       0.18 × 10⁻³       1.189         3210° R (1782 K)       0.21 × 10⁻³       1.314         3460° R (1923 K)       0.24 × 10⁻³       1.502         3960° R (2200 K)       0.33 × 10⁻³       2.065         4460° R (2478 K)       0.48 × 10⁻³       3.002         4710° R (2617 K)       0.48 × 10⁻³       3.002         4960° R (2756 K)       0.56 × 10⁻³       3.502         5960° R (3311 K)       0.78 × 10⁻³       4.880         5960° R (3311 K)       0.78 × 10⁻³       4.880         5960° R (3311 K)       1.02 × 10⁻³       6.390         6400° R (3555 K)       1.18 × 10⁻³       7.380         6800° R (3778 K)       1.02 × 10⁻³	49600 R	(2756 K)		 	 	 	:										0.525	2.19
5960° R (3311 K)       0.535       2.24         6460° R (3590 K)       0.540       2.26         6960° R (3867 K)       0.545       2.28         Thermal conductivity:       Btu/ft-sec-°R       W/m-K         500° R (278 K)       0.13 × 10 <sup>-3</sup> 0.810         1000° R (556 K)       0.14 × 10 <sup>-3</sup> 0.872         1460° R (811 K)       0.15 × 10 <sup>-3</sup> 0.935         1960° R (1089 K)       0.16 × 10 <sup>-3</sup> 0.977         2460° R (1366 K)       0.18 × 10 <sup>-3</sup> 1.189         3210° R (1782 K)       0.21 × 10 <sup>-3</sup> 1.819         3210° R (1782 K)       0.21 × 10 <sup>-3</sup> 1.502         3960° R (1923 K)       0.24 × 10 <sup>-3</sup> 1.502         3960° R (2200 K)       0.33 × 10 <sup>-3</sup> 2.065         4460° R (2478 K)       0.48 × 10 <sup>-3</sup> 3.002         4960° R (2576 K)       0.48 × 10 <sup>-3</sup> 3.502         5960° R (3311 K)       0.48 × 10 <sup>-3</sup> 3.502         4660° R (3311 K)       0.78 × 10 <sup>-3</sup> 4.880         5960° R (3311 K)       0.78 × 10 <sup>-3</sup> 4.880         5960° R (3311 K)       1.02 × 10 <sup>-3</sup> 6.390         6400° R (3555 K)       1.18 × 10 <sup>-3</sup> 7.380         6800° R (3778 K)	5460° R	(3030 K)		 	 	 											0.530	2.21
6460° R (3590 K)       0.540       2.26         6960° R (3667 K)       0.545       2.28         Thermal conductivity:       Btu/ft-sec-oR       W/m-K         500° R (278 K)       0.13 × 10 <sup>-3</sup> 0.810         1000° R (556 K)       0.14 × 10 <sup>-3</sup> 0.872         1460° R (811 K)       0.15 × 10 <sup>-3</sup> 0.935         1960° R (1089 K)       0.16 × 10 <sup>-3</sup> 0.977         2460° R (1366 K)       0.18 × 10 <sup>-3</sup> 1.128         2960° R (1645 K)       0.19 × 10 <sup>-3</sup> 1.189         3210° R (1782 K)       0.21 × 10 <sup>-3</sup> 1.314         3460° R (1923 K)       0.24 × 10 <sup>-3</sup> 1.502         3960° R (1290 K)       0.33 × 10 <sup>-3</sup> 2.065         4460° R (2478 K)       0.43 × 10 <sup>-3</sup> 3.002         4960° R (2478 K)       0.48 × 10 <sup>-3</sup> 3.002         4960° R (256 K)       0.56 × 10 <sup>-3</sup> 3.502         4560° R (3331 K)       0.76 × 10 <sup>-3</sup> 4.880         5960° R (3311 K)       1.02 × 10 <sup>-3</sup> 6.390         6400° R (3778 K)       1.09 × 10 <sup>-3</sup> 9.325         Char surface emissivity       0.7         Char heat of sublimation       9000 Btu/bm (0.288 MJ/kg)         Char surface kinetics;	5960° R	(3311 K)		 	 	 											0.535	2.24
Thermal conductivity:         Btu/ft-sec-oR         W/m-K           500° R (278 K)         0.13 × 10 <sup>-3</sup> 0.810           1000° R (556 K)         0.14 × 10 <sup>-3</sup> 0.872           1460° R (811 K)         0.15 × 10 <sup>-3</sup> 0.935           1960° R (1089 K)         0.16 × 10 <sup>-3</sup> 0.977           2460° R (1366 K)         0.18 × 10 <sup>-3</sup> 1.128           2960° R (1645 K)         0.19 × 10 <sup>-3</sup> 1.189           3210° R (1782 K)         0.21 × 10 <sup>-3</sup> 1.314           3460° R (1923 K)         0.24 × 10 <sup>-3</sup> 1.502           3960° R (2200 K)         0.24 × 10 <sup>-3</sup> 2.065           4460° R (2478 K)         0.43 × 10 <sup>-3</sup> 2.790           4710° R (2617 K)         0.48 × 10 <sup>-3</sup> 3.002           4960° R (3766 K)         0.78 × 10 <sup>-3</sup> 4.880           5960° R (3311 K)         0.78 × 10 <sup>-3</sup> 4.880           5960° R (3311 K)         1.02 × 10 <sup>-3</sup> 6.390           6400° R (3555 K)         1.18 × 10 <sup>-3</sup> 7.380           6800° R (3778 K)         1.29 × 10 <sup>-3</sup> 6.390           Char surface emissivity         0.7           Char heat of combustion         5100 Btu/bm (11.82 MJ/kg)           Char surface kinet																	0.540	2.26
500° R (278 K)       0.13 × 10 <sup>-3</sup> 0.810         1000° R (556 K)       0.14 × 10 <sup>-3</sup> 0.872         1460° R (811 K)       0.15 × 10 <sup>-3</sup> 0.995         1960° R (1089 K)       0.16 × 10 <sup>-3</sup> 0.977         2460° R (1366 K)       0.18 × 10 <sup>-3</sup> 1.128         2960° R (1645 K)       0.19 × 10 <sup>-3</sup> 1.189         3210° R (1782 K)       0.21 × 10 <sup>-3</sup> 1.314         3460° R (1923 K)       0.24 × 10 <sup>-3</sup> 1.502         3960° R (2200 K)       0.33 × 10 <sup>-3</sup> 2.065         4460° R (2478 K)       0.43 × 10 <sup>-3</sup> 3.002         4710° R (2617 K)       0.48 × 10 <sup>-3</sup> 3.002         4960° R (2756 K)       0.56 × 10 <sup>-3</sup> 3.502         5460° R (3331 K)       0.78 × 10 <sup>-3</sup> 4.880         5960° R (3311 K)       1.02 × 10 <sup>-3</sup> 6.390         6400° R (3778 K)       1.18 × 10 <sup>-3</sup> 7.380         6800° R (3778 K)       1.49 × 10 <sup>-3</sup> 9.325         Char surface emissivity       0.7         Char heat of combustion       5100 Btu/lbm (11.82 MJ/kg)         Char surface kinetics;       Frequency factor       4.47 × 10 <sup>4</sup> lbm/ft²-sec-atm¹/² (21.8 × 10 <sup>4</sup> kg/m²-s-atm¹/²)         Activation energy       42.3 kcal/mole (0.177 MJ/mo	6960° R	(3867 K)		 	 	 										(	0.545	2.28
500° R (278 K)       0.13 × 10 <sup>-3</sup> 0.810         1000° R (556 K)       0.14 × 10 <sup>-3</sup> 0.872         1460° R (811 K)       0.15 × 10 <sup>-3</sup> 0.995         1960° R (1089 K)       0.16 × 10 <sup>-3</sup> 0.977         2460° R (1366 K)       0.18 × 10 <sup>-3</sup> 1.128         2960° R (1645 K)       0.19 × 10 <sup>-3</sup> 1.189         3210° R (1782 K)       0.21 × 10 <sup>-3</sup> 1.314         3460° R (1923 K)       0.24 × 10 <sup>-3</sup> 1.502         3960° R (2200 K)       0.33 × 10 <sup>-3</sup> 2.065         4460° R (2478 K)       0.43 × 10 <sup>-3</sup> 3.002         4710° R (2617 K)       0.48 × 10 <sup>-3</sup> 3.002         4960° R (2756 K)       0.56 × 10 <sup>-3</sup> 3.502         5460° R (3331 K)       0.78 × 10 <sup>-3</sup> 4.880         5960° R (3311 K)       1.02 × 10 <sup>-3</sup> 6.390         6400° R (3778 K)       1.18 × 10 <sup>-3</sup> 7.380         6800° R (3778 K)       1.49 × 10 <sup>-3</sup> 9.325         Char surface emissivity       0.7         Char heat of combustion       5100 Btu/lbm (11.82 MJ/kg)         Char surface kinetics;       Frequency factor       4.47 × 10 <sup>4</sup> lbm/ft²-sec-atm¹/² (21.8 × 10 <sup>4</sup> kg/m²-s-atm¹/²)         Activation energy       42.3 kcal/mole (0.177 MJ/mo	Thermal c	onductivity:														Bhi /fi		W/m-K
1000° R (556 K)       0.14 × 10 <sup>-3</sup> 0.872         1460° R (811 K)       0.15 × 10 <sup>-3</sup> 0.935         1960° R (1089 K)       0.16 × 10 <sup>-3</sup> 0.977         2460° R (1366 K)       0.18 × 10 <sup>-3</sup> 1.128         2960° R (1645 K)       0.19 × 10 <sup>-3</sup> 1.189         3210° R (1782 K)       0.21 × 10 <sup>-3</sup> 1.314         3460° R (1923 K)       0.24 × 10 <sup>-3</sup> 1.502         3960° R (2200 K)       0.33 × 10 <sup>-3</sup> 2.065         4460° R (2478 K)       0.43 × 10 <sup>-3</sup> 2.790         4710° R (2617 K)       0.48 × 10 <sup>-3</sup> 3.002         4960° R (2756 K)       0.56 × 10 <sup>-3</sup> 3.502         5460° R (3303 K)       0.78 × 10 <sup>-3</sup> 4.880         5960° R (3311 K)       1.02 × 10 <sup>-3</sup> 6.390         6400° R (3555 K)       1.18 × 10 <sup>-3</sup> 7.380         6800° R (3778 K)       1.49 × 10 <sup>-3</sup> 9.325         Char surface emissivity       0.7         Char heat of combustion       5100 Btu/lbm (11.82 MJ/kg)         Char surface kinetics;       Frequency factor       4.47 × 10 <sup>4</sup> lbm/ft²-sec-atm1/2 (21.8 × 10 <sup>4</sup> kg/m²-s-atm1/2)         Activation energy       42.3 kcal/mole (0.177 MJ/mole)				 	 	 												,
1460° R (811 K)       0.15 × 10 <sup>-3</sup> 0.935         1960° R (1089 K)       0.16 × 10 <sup>-3</sup> 0.977         2460° R (1366 K)       0.18 × 10 <sup>-3</sup> 1.128         2960° R (1645 K)       0.19 × 10 <sup>-3</sup> 1.189         3210° R (1782 K)       0.21 × 10 <sup>-3</sup> 1.314         3460° R (1923 K)       0.24 × 10 <sup>-3</sup> 1.502         3960° R (2200 K)       0.33 × 10 <sup>-3</sup> 2.065         4460° R (2478 K)       0.43 × 10 <sup>-3</sup> 2.790         4710° R (2617 K)       0.48 × 10 <sup>-3</sup> 3.002         4960° R (2756 K)       0.56 × 10 <sup>-3</sup> 3.502         5460° R (3030 K)       0.78 × 10 <sup>-3</sup> 4.880         5960° R (3311 K)       1.02 × 10 <sup>-3</sup> 6.390         6400° R (3555 K)       1.18 × 10 <sup>-3</sup> 7.380         6800° R (3778 K)       1.149 × 10 <sup>-3</sup> 9.325         Char surface emissivity       0.7         Char heat of combustion       5100 Btu/lbm (11.82 MJ/kg)         Char surface kinetics;       Frequency factor       4.47 × 10 <sup>4</sup> lbm/ft²-sec-atm <sup>1/2</sup> (21.8 × 10 <sup>4</sup> kg/m²-s-atm <sup>1/2</sup> )         Activation energy       42.3 kcal/mole (0.177 MJ/mole)																		
1960° R (1089 K)       0.16 × 10 <sup>-3</sup> 0.977         2460° R (1366 K)       0.18 × 10 <sup>-3</sup> 1.128         2960° R (1645 K)       0.19 × 10 <sup>-3</sup> 1.189         3210° R (1782 K)       0.21 × 10 <sup>-3</sup> 1.314         3460° R (1923 K)       0.24 × 10 <sup>-3</sup> 1.502         3960° R (2200 K)       0.33 × 10 <sup>-3</sup> 2.065         4460° R (2478 K)       0.43 × 10 <sup>-3</sup> 2.790         4710° R (2617 K)       0.46 × 10 <sup>-3</sup> 3.002         4960° R (2756 K)       0.56 × 10 <sup>-3</sup> 3.502         5460° R (3030 K)       0.78 × 10 <sup>-3</sup> 4.880         5960° R (3311 K)       1.02 × 10 <sup>-3</sup> 6.390         6400° R (3555 K)       1.18 × 10 <sup>-3</sup> 7.380         6800° R (3778 K)       1.49 × 10 <sup>-3</sup> 9.325         Char surface emissivity       0.7         Char heat of combustion       5100 Btu/lbm (11.82 MJ/kg)         Char surface kinetics;       Frequency factor       4.47 × 10 <sup>4</sup> lbm/ft²-sec-atm <sup>1</sup> /2 (21.8 × 10 <sup>4</sup> kg/m²-s-atm <sup>1</sup> /2)         Activation energy       42.3 kcal/mole (0.177 MJ/mole)																		
24600 R (1366 K)       0.18 × 10 <sup>-3</sup> 1.128         29600 R (1645 K)       0.19 × 10 <sup>-3</sup> 1.189         32100 R (1782 K)       0.21 × 10 <sup>-3</sup> 1.314         34600 R (1923 K)       0.24 × 10 <sup>-3</sup> 1.502         39600 R (2200 K)       0.33 × 10 <sup>-3</sup> 2.065         44600 R (2478 K)       0.43 × 10 <sup>-3</sup> 2.790         47100 R (2617 K)       0.48 × 10 <sup>-3</sup> 3.002         49600 R (2756 K)       0.56 × 10 <sup>-3</sup> 3.502         54600 R (3030 K)       0.78 × 10 <sup>-3</sup> 4.880         59600 R (3311 K)       1.02 × 10 <sup>-3</sup> 6.390         64000 R (3555 K)       1.18 × 10 <sup>-3</sup> 7.380         68000 R (3778 K)       1.49 × 10 <sup>-3</sup> 9.325         Char surface emissivity       0.7         Char heat of combustion       5100 Btu/lbm (11.82 MJ/kg)         Char surface kinetics;       9000 Btu/lbm (20.88 MJ/kg)         Char surface kinetics;       Frequency factor       4.47 × 10 <sup>4</sup> lbm/ft²-sec-atm¹/2 (21.8 × 10 <sup>4</sup> kg/m²-s-atm¹/2)         Activation energy       42.3 kcal/mole (0.177 MJ/mole)																		
2960° R (1645 K)       0.19 × 10-3       1.189         3210° R (1782 K)       0.21 × 10-3       1.314         3460° R (1923 K)       0.24 × 10-3       1.502         3960° R (2200 K)       0.33 × 10-3       2.065         4460° R (2478 K)       0.43 × 10-3       2.790         4710° R (2617 K)       0.48 × 10-3       3.002         4960° R (2756 K)       0.56 × 10-3       3.502         5460° R (3030 K)       0.78 × 10-3       4.880         5960° R (3311 K)       1.02 × 10-3       6.390         6400° R (3555 K)       1.18 × 10-3       7.380         6800° R (3778 K)       1.49 × 10-3       9.325         Char surface emissivity       0.7         Char heat of combustion       5100 Btu/lbm (11.82 MJ/kg)         Char surface kinetics;       9000 Btu/lbm (20.88 MJ/kg)         Char surface kinetics;       Frequency factor       4.47 × 10 <sup>4</sup> lbm/ft²-sec-atm¹/2 (21.8 × 10 <sup>4</sup> kg/m²-s-atm¹/2)         Activation energy       42.3 kcal/mole (0.177 MJ/mole)																		
3210° R (1782 K)       0.21 × 10-3       1.314         3460° R (1923 K)       0.24 × 10-3       1.502         3960° R (2200 K)       0.33 × 10-3       2.065         4460° R (2478 K)       0.43 × 10-3       2.790         4710° R (2617 K)       0.48 × 10-3       3.002         4960° R (2756 K)       0.56 × 10-3       3.502         5460° R (3030 K)       0.78 × 10-3       4.880         5960° R (3311 K)       1.02 × 10-3       6.390         6400° R (3555 K)       1.18 × 10-3       7.380         6800° R (3778 K)       1.49 × 10-3       9.325         Char surface emissivity       0.7         Char heat of combustion       5100 Btu/lbm (11.82 MJ/kg)         Char surface kinetics;       9000 Btu/lbm (20.88 MJ/kg)         Char surface kinetics;       Frequency factor       4.47 × 10 <sup>4</sup> lbm/ft²-sec-atm²/2 (21.8 × 10 <sup>4</sup> kg/m²-s-atm²/2)         Activation energy       42.3 kcal/mole (0.177 MJ/mole)																		1.189
3960° R (2200 K)       0.33 × 10⁻³       2.065         4460° R (2478 K)       0.43 × 10⁻³       2.790         4710° R (2617 K)       0.48 × 10⁻³       3.002         4960° R (2756 K)       0.56 × 10⁻³       3.502         5460° R (3030 K)       0.78 × 10⁻³       4.880         5960° R (3311 K)       1.02 × 10⁻³       6.390         6400° R (3555 K)       1.18 × 10⁻³       7.380         6800° R (3778 K)       1.49 × 10⁻³       9.325         Char surface emissivity       0.7         Char heat of combustion       5100 Btu/lbm (11.82 MJ/kg)         Char heat of sublimation       9000 Btu/lbm (20.88 MJ/kg)         Char surface kinetics;       Frequency factor       4.47 × 10⁴ lbm/ft²-sec-atm¹/2 (21.8 × 10⁴ kg/m²-s-atm¹/2)         Activation energy       42.3 kcal/mole (0.177 MJ/mole)																		1.314
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	3460° R	(1923 K)		 	 	 	. : .		:							0.24	× 10-3	1.502
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	3960° R	(2200 K)		 	 	 										0.33	$\times$ 10 <sup>-3</sup>	2.065
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	4460° R	(2478 K)		 	 	 										0.43	× 10-3	2.790
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	4710° R	(2617 K)		 	 	 										0.48	$\times$ 10 <sup>-3</sup>	3.002
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$4960^{\circ}$ R	(2756 K)		 	 	 										0.56	$\times$ 10 <sup>-3</sup>	3.502
6400° R (3555 K). 1.18 × 10 <sup>-3</sup> 7.380 6800° R (3778 K). 1.49 × 10 <sup>-3</sup> 9.325  Char surface emissivity . 0.7  Char heat of combustion 5100 Btu/lbm (11.82 MJ/kg)  Char heat of sublimation 9000 Btu/lbm (20.88 MJ/kg)  Char surface kinetics;  Frequency factor 4.47 × 10 <sup>4</sup> lbm/ft <sup>2</sup> -sec-atm <sup>1</sup> /2 (21.8 × 10 <sup>4</sup> kg/m <sup>2</sup> -s-atm <sup>1</sup> /2)  Activation energy 42.3 kcal/mole (0.177 MJ/mole)	5460° R	(3030 K)		 	 	 										0.78	$\times$ 10 <sup>-3</sup>	4.880
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	5960° R	(3311 K)		 	 	 										1.02	$\times$ 10 <sup>-3</sup>	6.390
	6400° R	(3555 K)		 	 	 										1.18	$\times$ 10 <sup>-3</sup>	7.380
Char heat of combustion       5100 Btu/lbm (11.82 MJ/kg)         Char heat of sublimation       9000 Btu/lbm (20.88 MJ/kg)         Char surface kinetics;       Frequency factor         Frequency factor       4.47 × 10 <sup>4</sup> lbm/ft <sup>2</sup> -sec-atm <sup>1</sup> /2 (21.8 × 10 <sup>4</sup> kg/m <sup>2</sup> -s-atm <sup>1</sup> /2)         Activation energy       42.3 kcal/mole (0.177 MJ/mole)	6800° R	(3778 K)		 	 	 										1.49	$\times$ 10 <sup>-3</sup>	9.325
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	Char surfac	ce emissivity	·	 	 	 											· · · · ·	0.7
Char surface kinetics;  Frequency factor	Char heat o	of combustion		 	 	 										5100 E	stu/lbm	(11.82 MJ/kg)
Frequency factor																		
Frequency factor	Char surfac	ce kinetics:																
Activation energy				 	 	 		. 4.	47 ×	104 1	lbm/	ft2-s	ec-	itm1	/2	(21.8 ×	104 kg/	m2-s-atm1/21
Itelaction of act																		

TABLE VI. - THERMAL PROPERTIES USED IN COMPUTER PREDICTIONS - Concluded (c) Pyrolysis gas

Specific heat:		Btu/lbm-OR kJ/kg-K
5000 B (970 K)		. 0.75 3.14
10000 D (556 K)		. 1.00 4.18
1000° R (050 K)		. 1.50 6.28
1460° R (817 K)		. 2.00 8.36
1960° R (1089 K)	,	. 1.00 4.18
2460° R (1366 K)		
2960° R (1645 K)		
3460° R (1923 K)		. 2.00
3960° R (2200 K)		
4460° R (2478 K)		
4960° R (2756 K)		. 2.00
5460° R (3030 K)		
5960° R (3311 K)		. 7.50 31.40
6460° R (3590 K)		. 9.50 39.75
6960° R (3867 K)		. 10.00 41.84

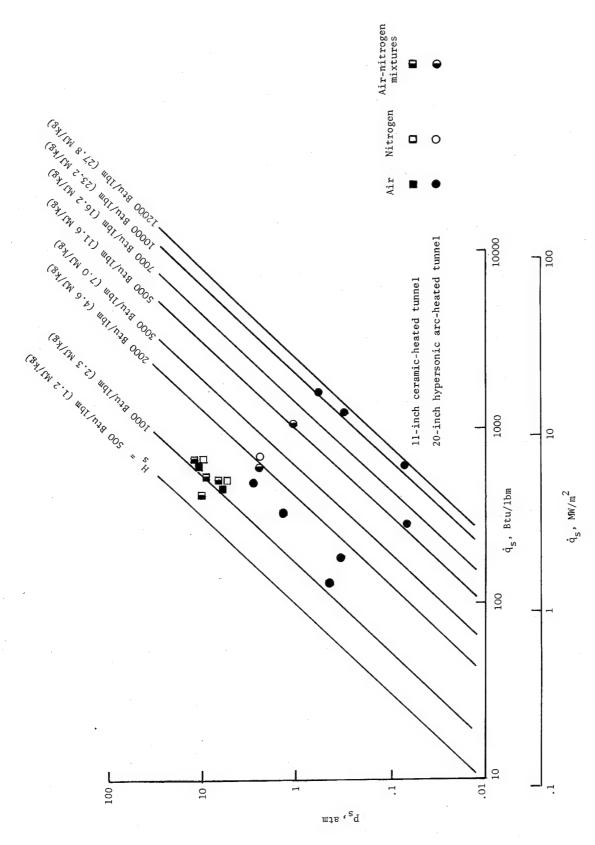


Figure 1.- Test conditions for a 1-inch-diameter (2.54 cm) hemispherical model.

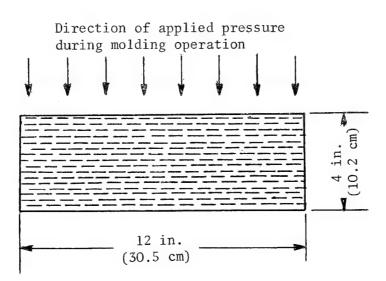
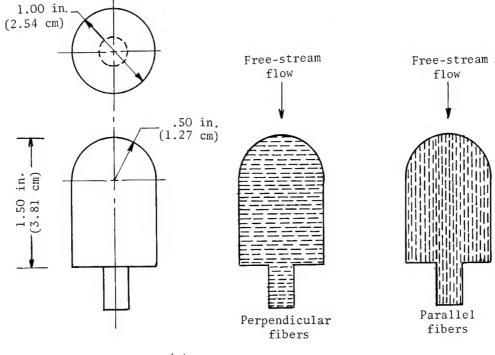
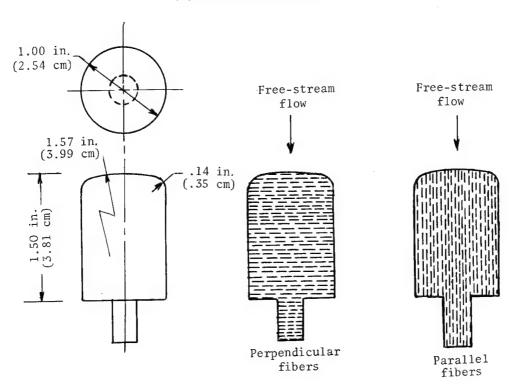


Figure 2.- Sketch of fiber orientation in molded billets.

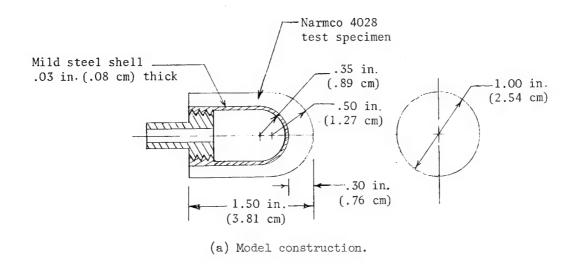


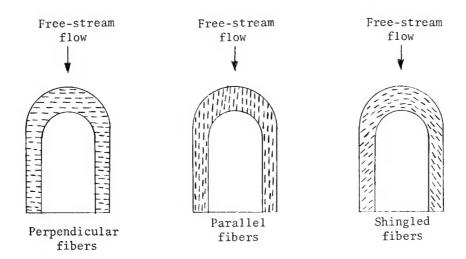
(a) Hemispherical nose.



(b) Blunt nose.

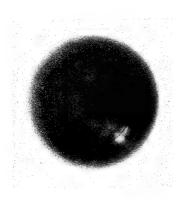
Figure 3.- Model design used for the study of the general behavior of the material.





(b) Fiber orientation in test specimen.

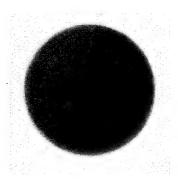
Figure 4.- Model design used to study the effect of fiber orientation.



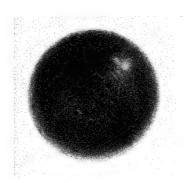
No holes



1 hole

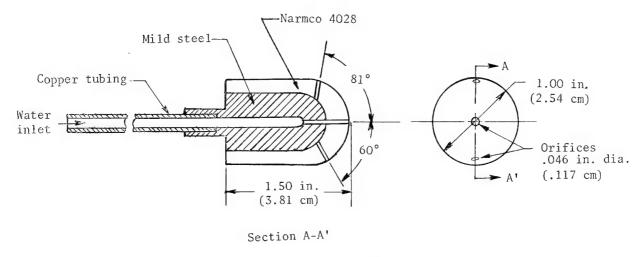


4 holes



13 holes

L-70-4707
Figure 5.- Photographs of the top view of the models used in the study of the effect of holes in the material. The holes were drilled in the hemispherical models shown in figure 3(a) with perpendicular-fiber orientation.



(a) Stagnation-point injection.

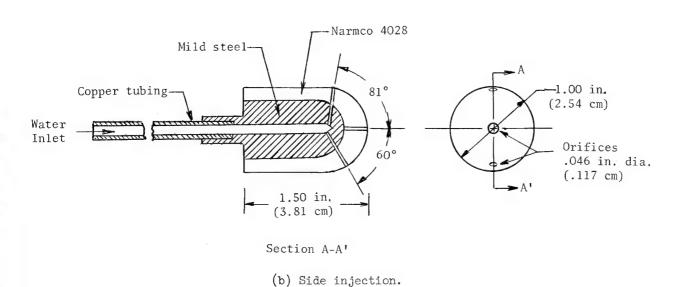
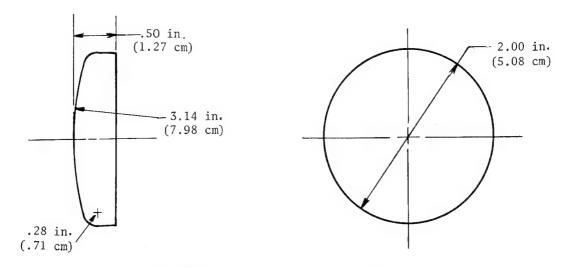
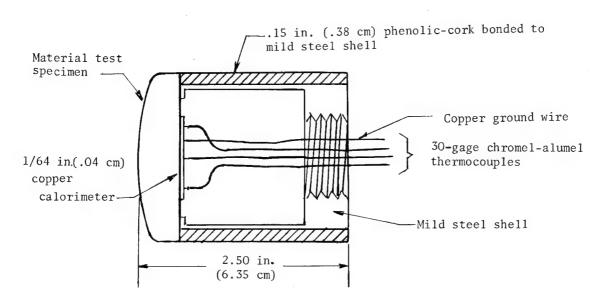


Figure 6.- Model design used to study the effect of water injection. Test specimen had shingled-fiber orientation as shown in figure 4(b).



(a) Shape of material test specimen.



(b) Material specimen and thermocouple assembly.

Figure 7.- Model design used in the evaluation of the thermal properties.







- (a) Hemispherical-nose model.  $p_{S} = 2.40 \text{ atm}; \quad K_{O} = 0.25.$   $\dot{q}_{S} = 700 \text{ Btu/ft}^{2}\text{-sec}$   $(7.95 \text{ MW/m}^{2});$   $H_{S} = 2340 \text{ Btu/lbm}$  (5.45 MJ/kg).
- (b) Blunt-nose model.  $p_{\rm S} = 10.41~{\rm atm;}~K_{\rm O} = 0.13; \\ \dot{q}_{\rm S} = 400~{\rm Btu/ft2-sec} \\ (4.54~{\rm MW/m^2}); \\ H_{\rm S} = 1100~{\rm Btu/lbm} \\ (2.55~{\rm MJ/kg}).$
- (c) Hemispherical-nose model.  $p_{\rm S} = 11.26~{\rm atm;}~{\rm K}_{\rm O} = 0.09;$   $\dot{q}_{\rm S} = 620~{\rm Btu/ft}^2-{\rm sec}$   $(7.04~{\rm MW/m}^2);$   $H_{\rm S} = 1100~{\rm Btu/lbm}$   $(2.55~{\rm MJ/kg}).$
- Figure 8.- Photographs showing mechanical char removal from the models during testing. Model design as shown in figure 5 with perpendicular-fiber orientation.

Nose shape
Blunt Hemisphere

Mechanical char removal □ ○

No mechanical char removal ■

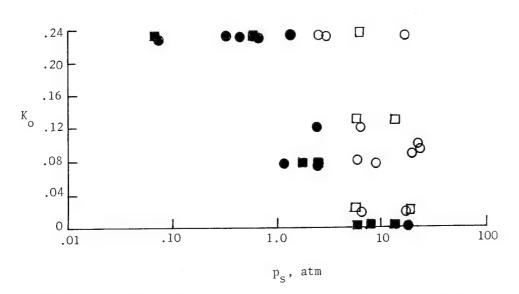


Figure 9.- Test environments at which mechanical char removal occurred. Fiber orientation in the material was perpendicular to the free-stream flow.

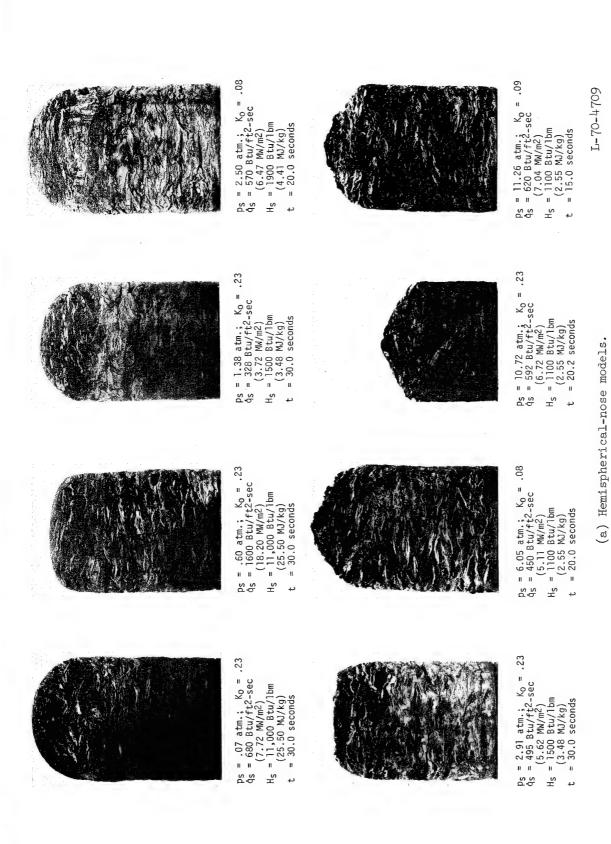


Figure 10.- Photographs of representative models showing the regime of mechanical char removal. Fiber orientation in the material was perpendicular to the free-stream flow.

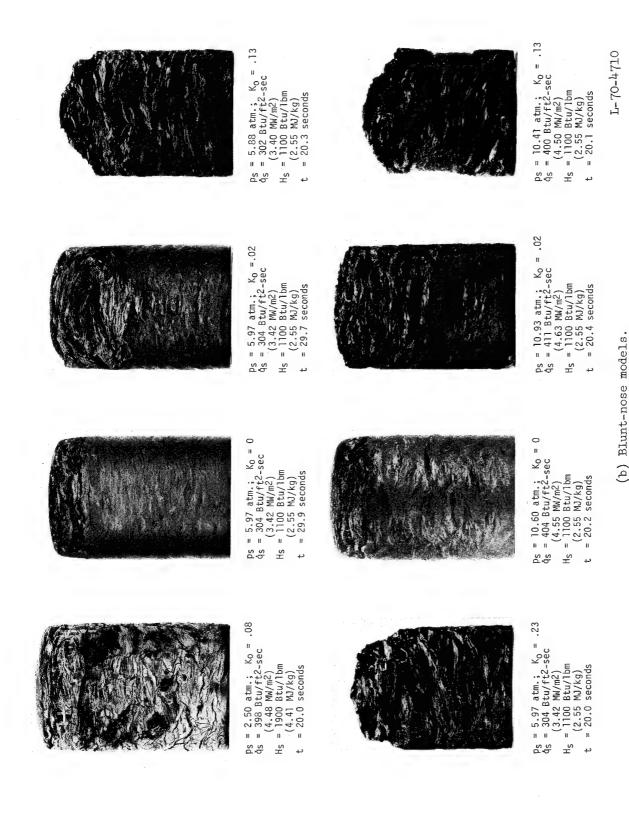
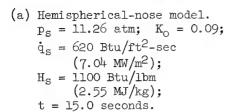
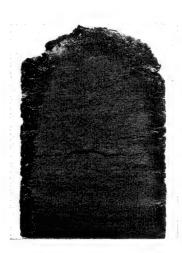


Figure 10. - Concluded.

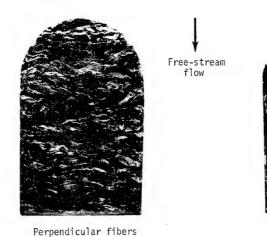






(b) Blunt-nose model.  $p_s = 5.88 \text{ atm}$ ;  $K_o = 0.13$ ;  $\dot{q}_s = 302 \text{ Btu/ft}^2\text{-sec}$   $(3.42 \text{ MW/m}^2)$ ;  $H_s = 1100 \text{ Btu/lbm}$  (2.55 MJ/kg); t = 20.3 seconds.

Figure 11.- Photographs of sectioned models showing the char thickness for models which experienced mechanical char removal.

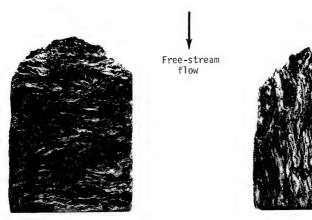


Parallel fibers

(a)  $p_s = 6.05 \text{ atm}; K_o = 0.08;$ 

 $\dot{q}_s = 450 \text{ Btu/ft}^2 - \text{sec } (5.18 \text{ MW/m}^2);$ 

 $H_S = 1100 \text{ Btu/lbm } (2.55 \text{ MJ/kg});$  t = 15.0 seconds.



Perpendicular fibers

Parallel fibers

L-70-4712 (b)  $p_s = 11.26 \text{ atm}$ ;  $K_o = 0.09$ ;  $\dot{q}_s = 620 \text{ Btu/ft}^2\text{-sec }(7.04 \text{ MW/m}^2)$ ;  $H_s = 1100 \text{ Btu/lbm }(2.55 \text{ MJ/kg})$ ; t = 15.0 seconds.

Figure 12.- Photographs of representative models (after testing) showing the effect of perpendicular- and parallel-fiber orientation on the behavior of the material. Models are of the hemispherical-nose design as shown in figure 3.

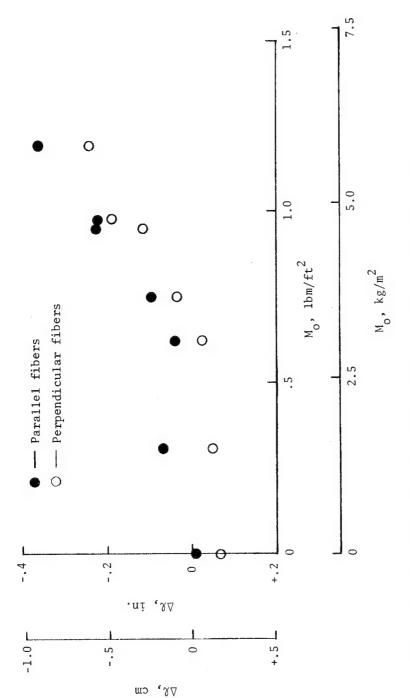
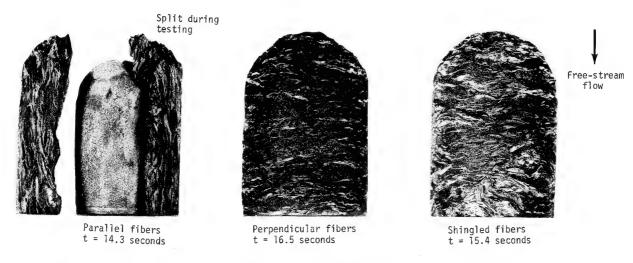
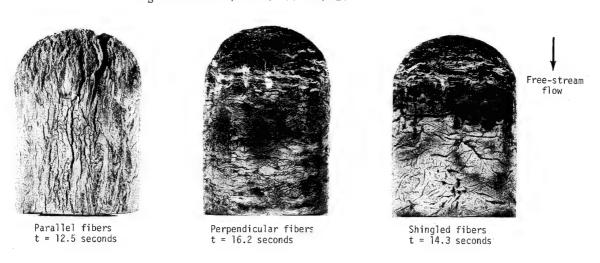


Figure 13.- The stagnation-point length change comparison for models with parallel- and perpendicular-fiber orientation tested at comparable conditions. The abscissa coordinate is the total cold-wall oxygen mass flux.



(a)  $p_s = 6.05$  atm;  $K_o = 0.08$ ;  $\dot{q}_s = 450$  Btu/ft<sup>2</sup>-sec (5.11 MW/m<sup>2</sup>);  $H_s = 1100$  Btu/1bm (2.55 MJ/kg).



(b)  $p_s = 2.50 \text{ atm}$ ;  $K_o = 0.12$ ;  $q_s = 600 \text{ Btu/ft}^2\text{-sec}$  (6.81 MW/m<sup>2</sup>);  $H_s = 1950 \text{ Btu/lbm}$  (4.53 MJ/kg).

Figure 14.- Photographs of representative models (after testing) showing the effect of three different fiber orientations on the behavior of the material. Models are of the design shown in figure 4.

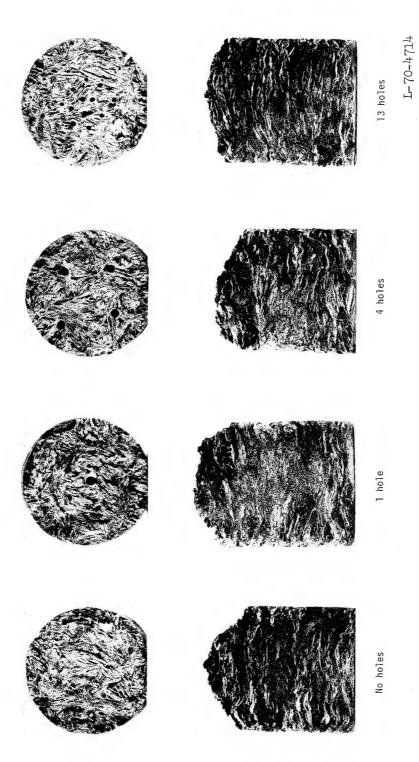
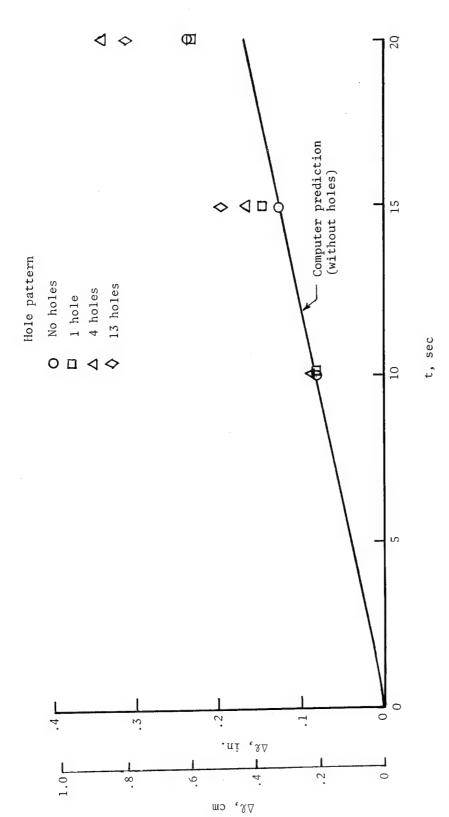
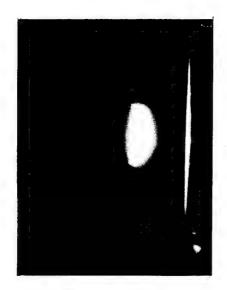


Figure 15.- Photographs of models (after testing) showing the effect of hole patterns in the material at the highest pressure test condition.  $p_S=11$  atm;  $K_O=0.10$ ;  $\dot{q}_S=610$  Btu/ft²-sec (6.93 MW/m²);  $H_S=1100$  Btu/lbm (2.55 MJ/kg); t=20.0 seconds.



 $\dot{q}_{\rm S}$  = 610 Btu/ft2-sec (6.95 MW/m<sup>2</sup>); H<sub>S</sub> = 1100 Btu/lbm (2.55 MJ/kg). Figure 16.- The stagnation-point recession for the models with hole patterns at the highest pressure test condition.  $p_S = 11 \text{ atm}$ ;  $K_O = 0.10$ ;

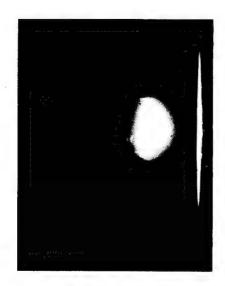


Between water pulses



During a water pulse  $\dot{w}$ =.059 lbm/sec (.027 kg/s)

## (a) Stagnation-point injection.



Between water pulses

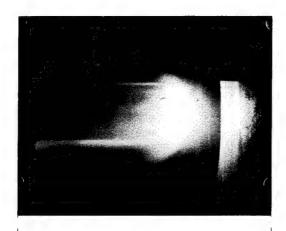


During a water pulse  $\psi$ =.135 lbm/sec (.061 kg/s)

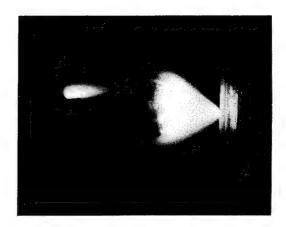
(b) Side-wall injection.

L-70-4715

Figure 17.- Photographs of the water-injection models during a test at the high-pressure test condition.  $p_{\rm S}$  = 11 atm;  $K_{\rm O}$  = 0.10;  $\dot{q}_{\rm S}$  = 610 Btu/ft<sup>2</sup>-sec (6.95 MW/m<sup>2</sup>);  $H_{\rm S}$  = 1100 Btu/lbm (2.55 MJ/kg).

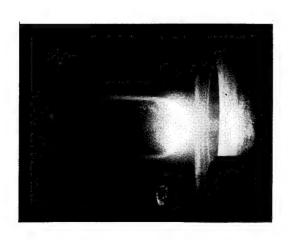


Between water pulses

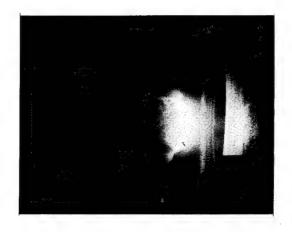


During a water pulse  $\dot{w}$ =.024 lbm/sec (.011 kg/s)

## (a) Stagnation-point injection.



Between water pulses



During a water pulse  $\psi$ =.035 lbm/sec (.016 kg/s)

(b) Sidewall injection.

(b) Sidewall injection.

L-70-4716

Figure 18.- Photographs of the water-injection models during a test at the low-pressure test condition.  $p_{\rm S}$  = 0.60 atm;  $K_{\rm O}$  = 0.232;  $\dot{q}_{\rm S}$  = 1600 Btu/ft<sup>2</sup>-sec (18.2 MW/m<sup>2</sup>);  $H_{\rm S}$  = 11 000 Btu/lbm (25.5 MJ/kg).

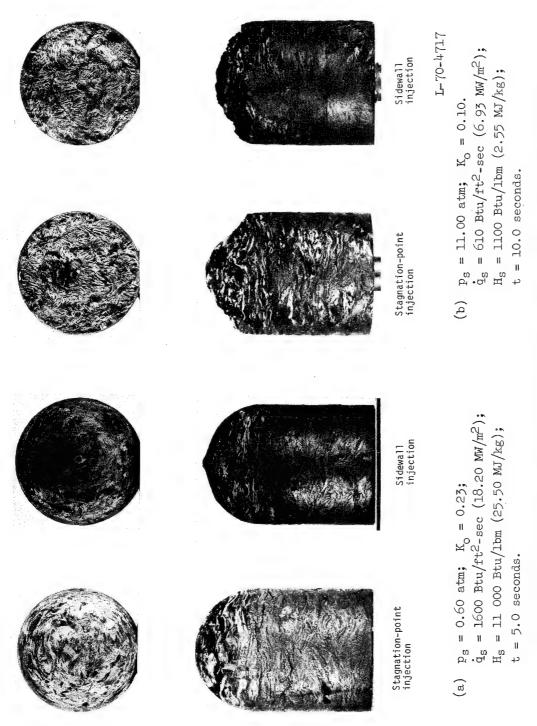
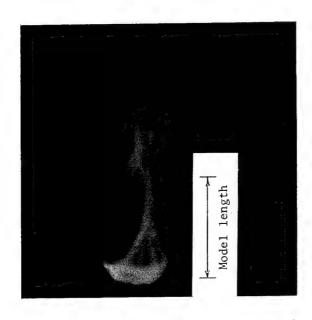
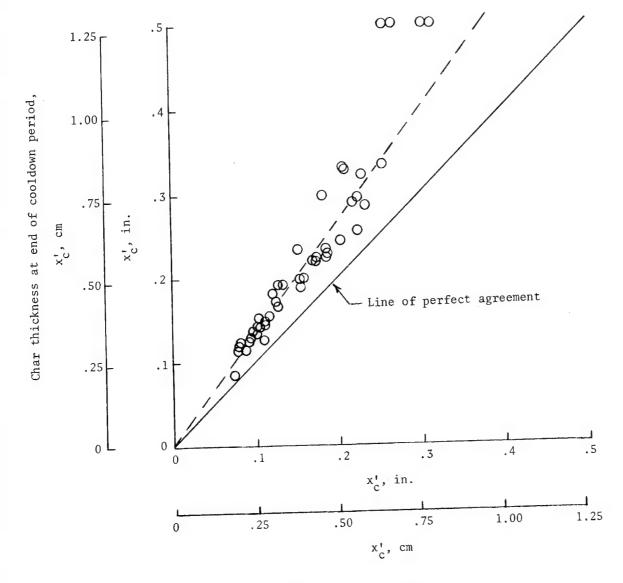


Figure 19.- Photographs of the water-injection models (after testing) from both the low-pressure and the high-pressure test conditions.



I-70-4718
Figure 20.- Photograph showing flaming of the model after retraction from stream in the ll-inch ceramicheated tunnel.



Char thickness at end of model exposure time

Figure 21.- The comparison from computer predictions of the stagnation-point char thicknesses at the end of model exposure time and at the end of the cooldown period.

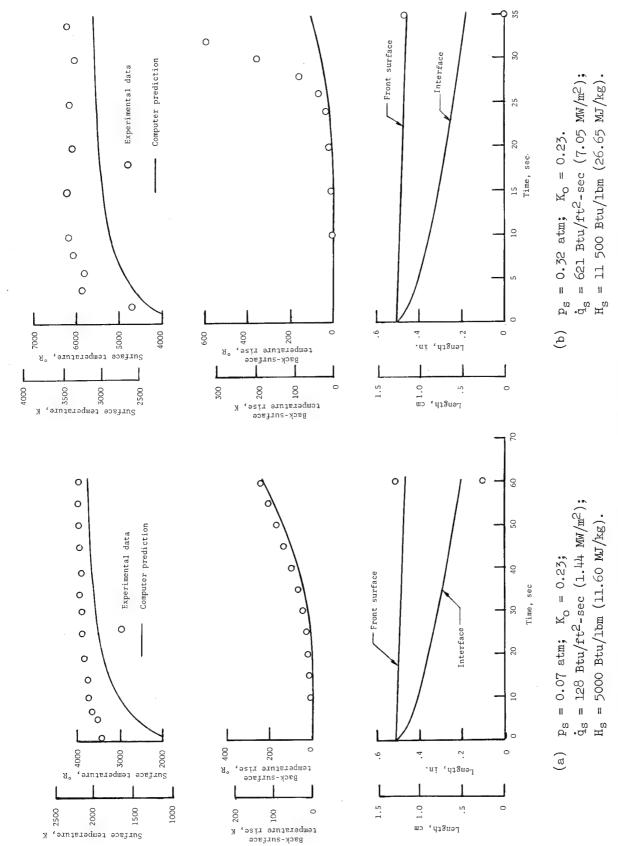


Figure 22. - Typical comparisons between experimental results and computer predictions for model design shown in figure 7.

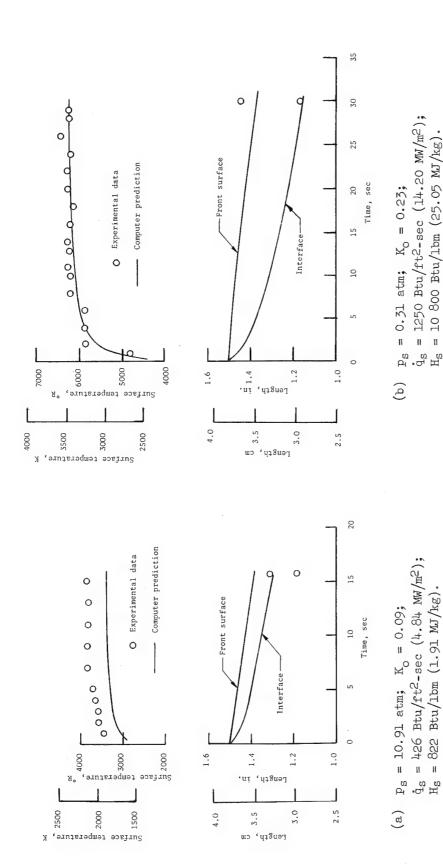


Figure 23.- Typical comparisons between experimental results and computer predictions for model design shown in figure 3(a).

 $\dot{q}_{\rm S} = 1250~{\rm Btu/ft^2\_sec}~(14.20~{\rm MW/m^2});$   $H_{\rm S} = 10~800~{\rm Btu/lbm}~(25.05~{\rm MJ/kg}).$ 

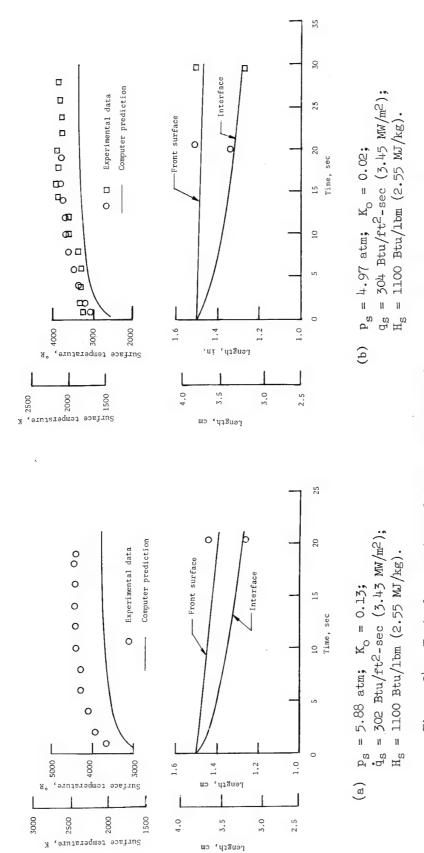
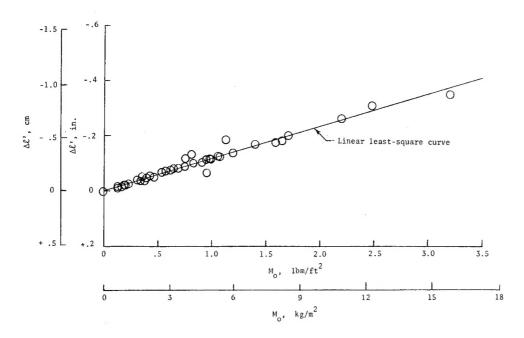
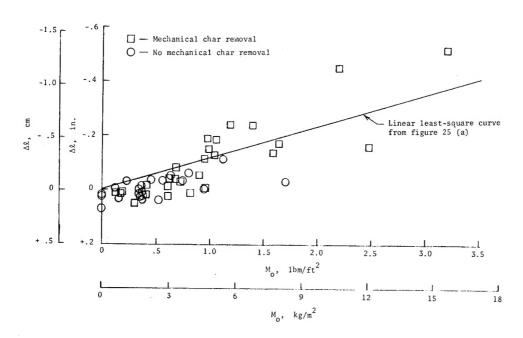


Figure 24. - Typical comparisons between experimental results and computer predictions for model design shown in figure 5(b).



(a) Results from computer predictions.



(b) Results from experimental data.

Figure 25.- Comparison between the experimental results and the computer predictions of model stagnation-point length change as a function of total cold-wall oxygen mass flux. The linear least-square curve is based on the results from the computer predictions.

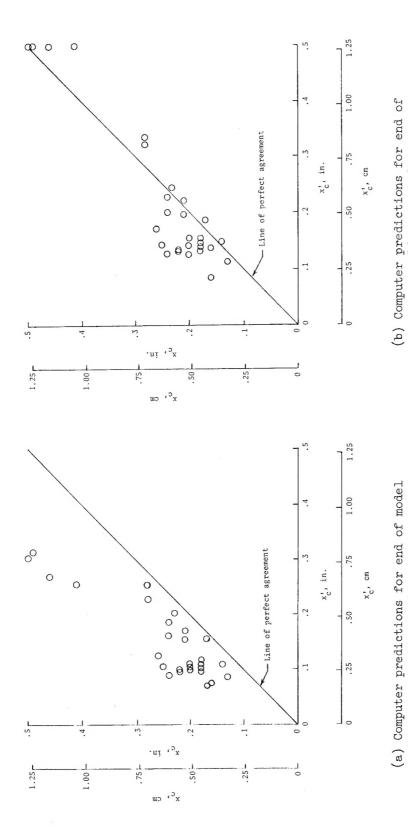


Figure 26.- The comparisons between the experimental data and the computer predictions for the stagnation-point char thicknesses. cooldown period. exposure time.

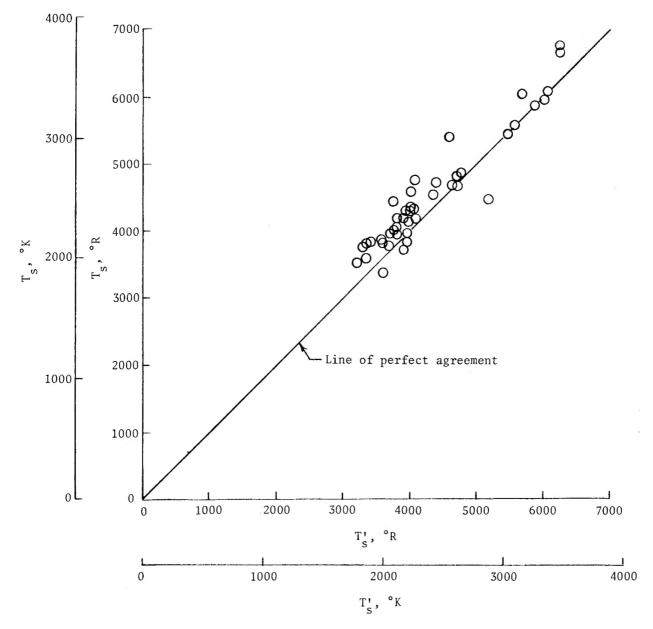


Figure 27.- The comparison between the experimental data and the computer predictions for the model stagnation-point surface temperature.

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